

# **AB 32 and the California Petroleum Refinery Sector**

## **Greenhouse Gas Reporting**

### **Technical Discussion**



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Sacramento**

# Discussion Topics

- **Reporting Basics**
- **Stationary Combustion – Fuels and Gases**
- **Process Emissions and Data**
- **Fugitives**
- **Reporting for Co-generation Facilities**
- **Verification**
- **Schedule**

# Proposed Reporting Basics

- Annual reporting on a facility basis
- Stationary combustion, process, fugitive emissions (direct emissions)
- Purchased energy usage (indirect emissions)
- Mobile sources  $\geq 25,000$  MT (not expected to affect refineries)
- All 6 Kyoto gases -- unless methods not specified in the regulation

# Defining the Facility

- Sources of GHGs on contiguous or adjacent properties
- Common operational control
  - Authority to implement environmental, health, safety rules
- A single major industrial source grouping (SIC/NAIC code)

# Potential for Broader Scope

- Market Advisory Committee draft report recommends broadest practical inclusion of sources, including transportation.
- “Mandatory reporting should be instituted as soon as possible for all entities likely to be covered by the program...”.
- ARB may need “a system to monitor the amount of carbon sold by refiners and importers in the form of gasoline and transport diesel fuel.”
- Should refineries report carbon content of products used in California?

# Stationary Combustion CO<sub>2</sub> Emissions Refinery Derived Fuel

## HHV – hourly

$$ECO_2 = F(\text{scf/time}) \times HHV(\text{Btu/scf}) \times EF(\text{tonnes C}/10^6 \text{ Btu}) \times 44/12$$

## Carbon Content – daily

$$ECO_2 = F(\text{m}^3/\text{time}) \times CF(\text{gmole}/\text{m}^3) \times M(\text{g}/\text{gmole}) \times C(\text{g C}/\text{g fuel}) \times 44/12 \\ \times \text{Mt}/10^6\text{g}$$

CF calculations will be used calculate the EF used in daily HHV emission calculations

ASTM Methods will be applied to HHV, flow rate and CF determinations

# Stationary Combustion CH<sub>4</sub> and N<sub>2</sub>O Emissions

- Equipment specific emission factors  
(AP-42, API, IPCC)
  - Refinery Gas – API equipment specific EFs

## CO<sub>2</sub> Emission Factors Natural Gas

HHV (Btu/scf)	Emission Factor (MT/10 <sup>9</sup> Btu)	
	CO <sub>2</sub>	Carbon
975 – 1,000	53.97	14.73
1,001 – 1,025	52.87	14.43
1,026 – 1,050	53.02	14.47
1,051 – 1,075	53.42	14.58
1,075 – 1,100	53.68	14.65
> 1,100	54.67	14.92

Source: EIA, Documentation for Emissions of Greenhouse Gases in the U.S. 2004, Dec 2006, DOE/EIA-0638(2004)

[www.eia.doe.gov/oiaf/1605/ggrpt/documentation/pdf/0638\(2004\).pdf](http://www.eia.doe.gov/oiaf/1605/ggrpt/documentation/pdf/0638(2004).pdf)

# Process Emissions

## Catalytic Cracking Units (CO<sub>2</sub>)

### (1) Coke Burn Method

USEPA 40 Part 63 (40CFR63.1564) refineries calculate coke burn rate (Rc)

$$ECO_2 = Rc \times CF \times [44 \text{ mass units of CO}_2 / 12 \text{ Mass units of C}]$$

### (2) Air rates and flue gas CO/CO<sub>2</sub> based method

$$ECO_2 = (AR + SOR) \times (FCO_2 + FCO) \times 44 / \text{molar conversion factor} \times 525,600 \text{ min/yr}$$

- CF = coke carbon fraction
- AR = air rate to regenerator
- SOR = supplemental O<sub>2</sub> rate
- FCO<sub>2</sub> = fraction of CO<sub>2</sub> in flue gas
- FCO = fraction of CO in flue gas

# Process Emissions

## Cokers (CO<sub>2</sub>)

$$E_{CO_2} = C_{rr} \times FC \times CO_2/C (44/12)$$

**Where:**

**$E_{CO_2}$  = CO<sub>2</sub> emissions (tonnes/yr)**

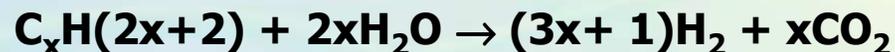
**$C_{rr}$  = cat regeneration rate (tonnes/yr)**

**FC = weigh fraction carbon on catalyst**

# Process Emissions

## Hydrogen Plant Production (CO<sub>2</sub>)

API Preferred Methods – 1) Mass balance or 2) H<sub>2</sub> production rate based  
H<sub>2</sub> production reaction



1)  $ECO_2 = FR \times CF \times 44g \text{ CO}_2/12g \text{ C}$  or

2)  $ECO_2 = H_2R \times (x \text{ mole CO}_2)/(3x + 1) \times 44/\text{molar volume conversion}$

**NOTE:** Method 2) does not apply w/ refinery gas where H<sub>2</sub> is a component of the fuel

FR = feedstock rate

CF = carbon fraction (fuel composition)

H<sub>2</sub>R = hydrogen production rate

X = stoichiometry derived from feedstock composition

# Process Emissions

## Hydrogen Plant Production (CO<sub>2</sub>)

- **Hydrogen plant feedstocks**
  - NG – HHV and CF w/Btu specific EFs
  - Refinery fuel – HHV hourly, CF daily
  - Fuel mixtures – naphtha – HHV hourly, CF daily
- **Hydrogen production rate (H2R)**
  - process data, hourly, do not use H2R method w/ refinery fuel
- **SMR Low Temperature Shift** – CO<sub>2</sub> desorber and de-aerator vent emissions

# Process Emissions

## Sulfur Recovery Units (CO<sub>2</sub>)

- **Stationary Combustion emissions**
  - Standard methods
  
- **Process emissions - Crude derived carbon entrained in the SRU process**
  - TGTU flow rate x CF in tail gas
  - $ECO_2 = \text{Sulfur production} \times 0.1374$

Source: Atmospheric Emissions Inventories Methodologies in the Petroleum Industry, ARPEL, 1998, pg. 6-39

<http://www.arpel.org/en/>

# Asphalt Blowing (CO<sub>2</sub> and CH<sub>4</sub>)

- Stationary Combustion emissions
  - Heaters, blowers – standard methodology
- Process emissions
  - Hot petroleum residuum emissions – Emission Factors and Flow Rate
  - Fugitive emissions from storage tanks, material handling operations – Model(s)?
  - Incinerators, thermal destruction devices – combustion fuel and crude derived VOCs

# Asphalt Blowing cont'd

- API Method (gas emissions x wt%)
  - AP-42 (1995)
  - 0.3 tonnes emissions/tonne blown asphalt
  - ARPEL (1998)
  - Tank head space vapor composition from 1980 reference

Calculation assumes no thermal destruction

CH<sub>4</sub> emitted as CH<sub>4</sub>

Does not calculate emissions for C<sub>2</sub>+ compounds (20 mole%)

# Process Data

## Data collection, archiving, and validation

### ■ Process Data

- Hydrogen production rate
- Coke burn rate
- Fuel composition data (HHV and CF)
- Flow rates
- SRU Tail Gas flow rates
- Asphalt production rates

# Fugitive Emissions

## Storage Tanks (CH<sub>4</sub>)

Fugitive CH<sub>4</sub> loss from crude oil storage tanks

- Working
- Breathing
- Flashing Losses
  
- Effect of wind speed on floating roof tank emissions
  
- E&P TANK equation of state estimates all three losses
  - Software available from API (\$450)

# Fugitive Emissions

## CH<sub>4</sub>

- **API – suggests that fugitive emissions are minimal**
  - **Model and Component based estimation methods**
- **New optical measurements suggest fugitive emissions may be larger, perhaps approaching 1-2% of total emissions**
- **Present methods may underestimate emissions**

[www.arc.ab.ca/ARC-Admin/UploadedDocs/Dial%20Final%20Report%20Nov06.pdf](http://www.arc.ab.ca/ARC-Admin/UploadedDocs/Dial%20Final%20Report%20Nov06.pdf)

**VOC Fugitive Losses: New Monitors, Emission Losses, and Potential Policy Gaps, 2006**  
International Workshop, EPA

[www.emsus.com/downloads/voc\\_fugitive\\_losses.pdf](http://www.emsus.com/downloads/voc_fugitive_losses.pdf)

# Fugitive Emissions

## Flares ( $\text{CO}_2$ , $\text{CH}_4$ , $\text{N}_2\text{O}$ )

- **AQMD Report data used to calculate emissions**
  - **Assume combustion efficiency (98-99.5%)**
  - **Conservative assumption concerning NMHC composition**

# Cogeneration: Proposed Approach



# Cogeneration Facilities in CA

- 917 Total (U.S. EPA data)
- 334 may be subject to reporting ( $\geq 1$  MW)
  - 201 facilities sell electricity
- 17 Sites at Petroleum Refineries in CA
  - All would be subject to reporting
  - Company with operational control would be responsible
- Reporting Requirements

# Cogeneration: Reporting Requirements

- Type of Facility
- Fuel Type and Amount Consumed
- CHP Technology Type(s)
- Total CO<sub>2</sub>, CH<sub>4</sub>, N<sub>2</sub>O
- Total electricity (MWh) output, sold to the grid, sold or provided to other users, and consumed on-site
- Total thermal energy (BTUs) output, usable thermal energy, and BTUs consumed on-site
- Indirect electricity purchases
- Emissions allocated based on energy stream output

# Cogeneration: GHG Emissions Allocation

- Stationary Combustion Emissions On-Site Reported as Direct Emissions
- Methods Evaluated
  - Work Potential
  - Energy Content
  - Public Utilities Commission (PUC) Conversion
  - Efficiency
- Considering Two Approaches
  - PUC Conversion Method
  - California Climate Action Registry (Registry) Efficiency Method

# PUC Conversion Method: GHG Emissions Allocation

$$\text{Emission Rate} = \frac{\text{Total GHG Emissions}}{\text{Electricity Output (kWh)} + \text{Usable Thermal Energy (kWh)}}$$

## Where:

Total GHG Emissions

= Metric Tons CO<sub>2</sub>e

Electricity Output

= Total Produced Annually

Thermal Energy Output

= Usable Thermal Energy\*

## Allocated Emissions:

Emissions<sub>Electricity</sub> = Emission Rate • Electricity Output

Emissions<sub>Thermal Energy</sub> = Total GHG Emissions – Emissions<sub>Electricity</sub>

\*FERC Definition: Thermal Energy Delivered to a Thermal Host

# PUC Conversion Method: Example Calculation

$$\text{Emission Rate} = \frac{\text{Total GHG Emissions}}{\text{Electricity Output (kWh)} + \text{Usable Thermal Energy (kWh)}}$$

## Where:

Total GHG Emissions	= 435,982 Metric Tons CO <sub>2</sub> e
Electricity Output	= 1,100,600 MWh
Usable Thermal Energy	= 2,710,000 million BTU
Emission Rate	= 0.00023 Metric Tons CO <sub>2</sub> e/kWh

## Allocated Emissions:

Energy Stream	Metric Tons CO <sub>2</sub> e
Electricity	253,138
Thermal Energy	182,844
Total	435,982

**Note: Example calculation uses API Compendium Assumptions & Input Data**

# Registry Efficiency Method: GHG Emissions Allocation

Thermal Energy	Electricity
$E_H = \frac{H/e_H}{H/e_H + P/e_P} \times E_T$	$E_P = E_T - E_H$

## Where:

$E_H$  = Emissions allocated to steam production

$H$  = Total steam (or heat) output (MMBtu)

$e_H$  = Efficiency of steam (or heat) production

$P$  = Total electricity output (MMBtu)

$e_P$  = Efficiency of electricity generation

$E_T$  = Total direct emissions of the CHP System

$E_P$  = Emissions allocated to electricity production

# Registry Efficiency Method: Example Calculation

$$E_H = \frac{\frac{3.614 \times 10^{12} \text{ BTU}}{0.80}}{\frac{3.614 \times 10^{12} \text{ BTU}}{0.80} + \frac{3.755 \times 10^{12} \text{ BTU}}{0.35}} \times 435,982 \text{ metric tons CO}_2\text{e}$$

## Where:

$E_H$  = Emissions allocated to steam production

$H$  =  $3.614 \times 10^{12}$  BTU

$e_H$  = 80% (Efficiency of steam production)

$P$  =  $3.755 \times 10^{12}$  BTU

$e_P$  = 35% (Efficiency of electricity generation)

$E_T$  = 435,982 metric tons  $\text{CO}_2\text{e}$

$E_P$  = Emissions allocated to electricity production

**$E_H$  = 129,186 metric tons  $\text{CO}_2\text{e}$**

**$E_P$  =  $435,982 - 129,186 = 306,982$  metric tons  $\text{CO}_2\text{e}$**

# Comparison of Methods: GHG Emissions Allocation

Energy Stream	PUC Conversion Method (Metric Tons CO <sub>2</sub> e)	Registry Efficiency Method (Metric Tons CO <sub>2</sub> e)
Electricity	253,138	306,796
Thermal Energy	182,844	129,186

# Cogeneration: Key Questions

- Should ARB adopt the PUC Conversion Method or the Registry's Efficiency Method?
- Do cogeneration facilities collect data on actual thermal energy and electricity production efficiency values?
- Are there any recommendations for ARB to adopt another method to allocate GHG emissions?
- Other comments?

# Verification: Initial Concepts



# Why Verification?



- AB 32 requires it
- Expected under international standards
- Experience with voluntary reporting shows the need
- Complexity of emissions estimation
- Critical for credibility of program

# Verification: Initial Proposal

- Require annual third-party verification for refineries, utilities, and power plants and co-generation facilities selling power to the grid or other users
- Require triennial third-party verification for cement plants and other stationary combustion sources  $\geq 25,000$  tons CO<sub>2</sub>
- Require annual third-party verification for anyone entering a future market

# Third Party Verification

- Consistent with existing standards, including ISO
  - Already required for CCAR members
  
- Verifiers to be trained under ARB approved curriculum
  - Demonstrated expertise
  - Consistency in verification

# Regulation to Specify

- Core GHG data verification requirements
- Accreditation requirements for verifiers
- Conflict-of-interest limitations
- ARB oversight

# Verification Activities

- Identify sources and review data management systems
- Focus on most significant and uncertain sources
- Differences exceeding 5 percent considered significant
- Detailed verification report to facility and ARB

# Reporting and Verification Timing

- Power Plants & Co-generators selling energy to other users
  - Emissions reports due by April 1
  - Verification complete by July 31
- Utilities, Refineries, Cement Plants and other stationary combustion sources
  - Emissions reports due by September 1
  - Verification complete by December 31

# Accreditation

- ARB to specify requirements necessary to become verifier
- Propose following fairly stringent international and CCAR approaches

# Conflict of Interest

- Term Limit
  - Verifiers to be changed after 3 years of conducting verification activities
  - Allowed to resume with client after 1 year off cycle for verification
- Conflict of Interest Policy
  - Must agree not to act on behalf of reporting facility as both consultant and verifier concurrently or within any 3 year period

# Verification Oversight

- ARB staff responsible for enforcing regulation
- Verification process will assist efforts to enforce compliance
- Targeted review of submitted data and verifiers

# Schedule

- CCAR Discussion Paper
  - Available for comment June 29, 2007 (tentative)
- Continued discussions with ARB staff working on regulatory language
  - Additional technical team meetings needed?
- Regulation Workshop
  - August 9, 2007

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***[www.arb.ca.gov/cc/cc.htm](http://www.arb.ca.gov/cc/cc.htm)***

