

NExBTL® Renewable Diesel Singapore Plant

FISH WASTE PATHWAY DESCRIPTION

1 INTRODUCTION

Neste Oil is the world's leading producer of Renewable Diesel with on-line capacity of 2 million metric tonnes per year (2 Mt/a) equivalent to 675 million gallons per annum (Mg/a) distributed between among its three world-wide facilities in Porvoo, Finland; Rotterdam, Holland and Singapore. Branded under the name of NExBTL®, this renewable diesel is a fungible, low-carbon, low-emission, paraffinic biofuel. Compared to petroleum diesel, NExBTL® has a higher cetane number and contains no aromatic compounds or sulphur. This translates into superior combustion properties to petroleum diesel.

This report outlines the NExBTL® Renewable Diesel production process as realized in the Neste Oil Singapore facility located at 1 Tuas South Lane, 637301 Singapore using fish waste feedstock. The Singapore refinery is built in the Tuas Industrial District, around 30 minutes from the center of Singapore. The refinery is integrated into the area's existing industrial infrastructure, and makes use of local site utilities and port and storage services.

2 FEEDSTOCK SUMMARY

Fish waste rendering and supply to the Neste Oil NExBTL® Renewable Diesel (RD) Singapore plant process is described. Fish waste is imported from Vietnam. Shipments vary by source and an average distance is calculated. Rendering energy consumption corresponds to the California low energy rendering process.

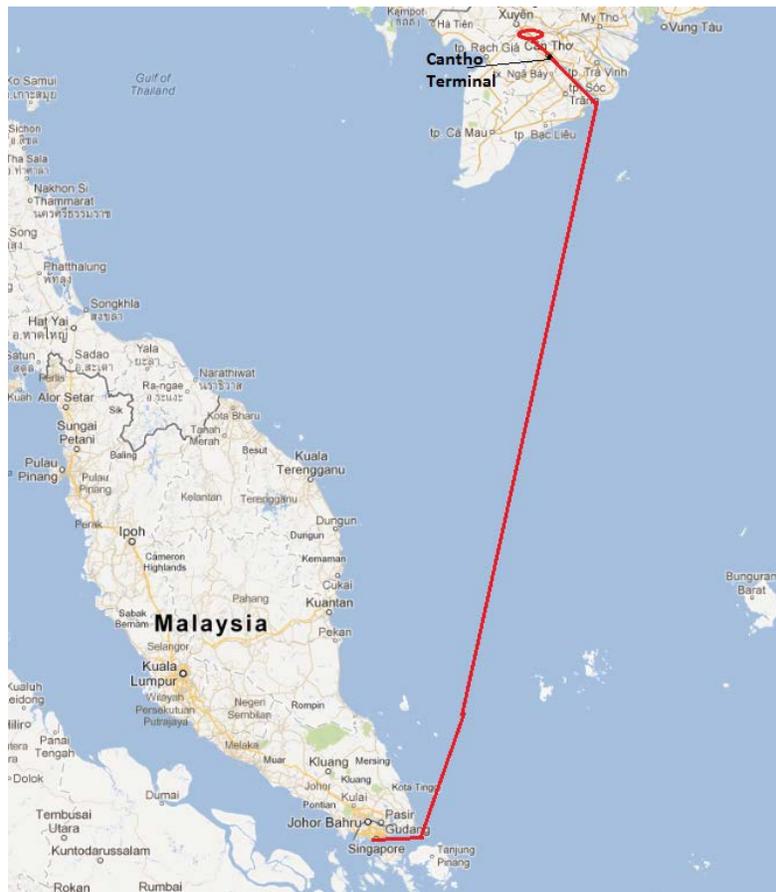
This report describes the tallow feed procurement and shipping to the NExBTL® Renewable Diesel production plant located in Singapore in Tuas Industrial District. This data was used to modify the CA-GREET model for the calculation of GHG emissions.

3 FEEDSTOCK PROCUREMENT

The fish waste to the Singapore plant is purchased from rendering facilities in Vietnam. The wastes are transported from various processing plants from the Mekong River to a terminal in Cantho City. The furthest transportation distance from a filleting site where the waste fish oil is separated to the Cantho terminal is approximately 50 miles. The transportation method is by truck.

The residual fish oil is then transported from Cantho City to the Neste Oil NExBTL® Singapore plant for processing using an ocean-going vessel with a distance of 585 nautical miles.

Figure 1



4 RENDERING PROCESS

The rendering of by-products from the fish industry is very similar to that of animal rendering processes in general. It consists of a number of process steps including cooking using steam, screw pressing, centrifuging and decanting (removing a top liquid layer from which a precipitate has settled). The cooking temperatures are selected in order to destroy microbes and remove water but not to denature the proteins. The main emissions are from raising steam. In Vietnam, the main fuel for the plants is rice husks which are available locally.

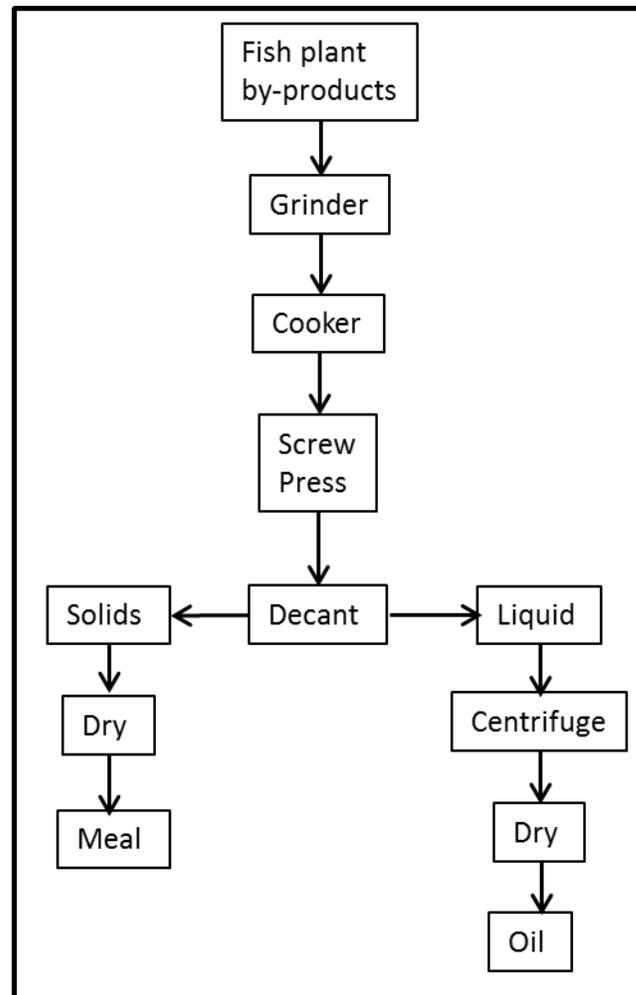
The raw materials used in the plant are the by-products or wastes from the fish filleting plant. They come from the fish plant, where the fish is be-headed, gutted, de-iced and de-scaled. It is then graded and filleted by hand. The fish fillet is then trimmed for blood, bones, fins, black membrane. By-products from the fillet production are then sent to the fish oil / meal factory for rendering.

The by-products enter the rendering facility where they are ground / mashed before being sent on to the pressure cooker. Steam is used to raise the temperature to over 100 C. The cooked raw material is then sent to a screw press before a 2 phase decanter clarifies the press water and separates the solids out. The liquid is centrifuged which further separates the protein meal from the oil. A block diagram of the overall process is shown below.

A final heating process at over 120 degrees Celsius for 2-2.5 hours removes remaining water from the fish oil. Temperatures are selected in order to destroy microbes and remove water but not to denature the proteins.

On a mass basis, for every tonne of by-products inputs, approximately 18% is fish meal, 24% is fish oil with the remainder water.

Most of the energy consumption in the rendering process is to raise steam for heating of the fish by-products and for water evaporation. The fuel most commonly used in Vietnam is rice husks.



An EU project from the 7th Framework Programme entitled Integrated Renewable Energy Solutions for Seafood Processing Stations found the energy consumption for fish oil processing plants to be:

Table 1. Consumption rates and costs of raw materials in fish waste oil extraction process.

Material	Daily rate	per ton of fish oil	Parameter	Cost/Profit	Parameter
Fish waste oil	17 ton	1.000 ton			
Fish cleaning waste	81 ton	4.765 ton	β_{fish}	100 €/ton	p_{fish}
Sold fish remains	18 ton	1.058 ton	λ_{remain}	280 €/ton	s_{remain}
Formid acid	2 ton	0.118 ton	β_{acid}	550 €/ton	p_{acid}
Heat	4000 kWh	235 kWh	θ_{fish}		
Electricity	700 kWh	41 kWh	$\varepsilon_{\text{fish}}$		

This Integrated Renewable Energy Solutions for Seafood Processing report is the best and only readily available data source of rendering energy consumption values. Such values from the demonstration project are reflective of the actual rendering consumption values based on the following reasons:

- The demonstration project is based on Pangasius farming in Vietnam;
- Neste Oil supplies from Pangasius processing facilities;
- The fish processing facilities do not separate energy consumption of refrigeration from the rest of the energy usage;
- Refrigeration or freezing the filets consumes most of the electricity; and
- Rendering energy is mostly from heat which is produced by burning rice husks and not a burden on the electricity consumption

Accordingly, these rendering energy consumption values described in the report have been used to calculate the carbon intensity for this pathway.

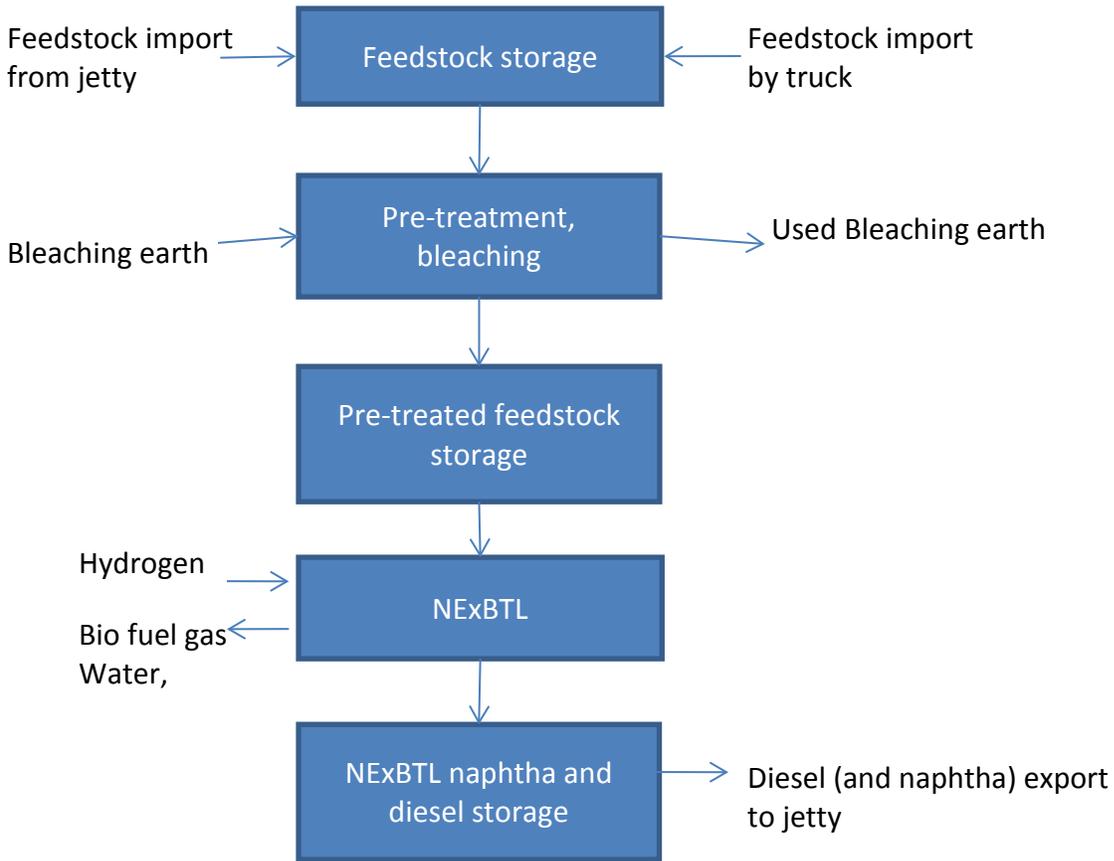
5 NExBTL® PROCESS OVERVIEW

The overall features of the Singapore NExBTL® Renewable Diesel production plant are shown in Figure 1. The process is comprised of a number of sub process units which are described in more detail below which are:

- Pre-treatment (impurities removal);
- Hydro treatment (oxygen removal, paraffins production and branching; propane production [high pressure and low pressure propane rich off gas])
- Stabilization (removal of residual light gases);
- Recycle (hydrogen recovered & recycled; water, carbon dioxide removal, light gases recovered)

The propane off gas from the Recycle section is used in the steam methane reformer (SMR) plant for the production of hydrogen and the propane off gas from the Stabilization section is used in a natural gas boiler to raise process steam.

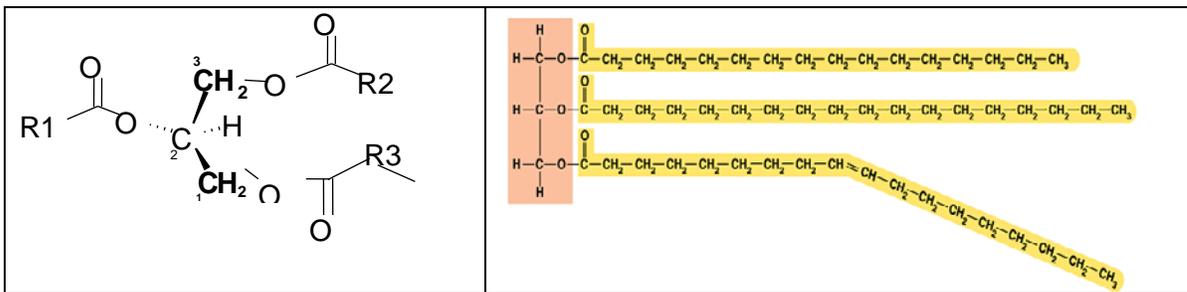
Figure 3
NExBTL® Singapore Process Diagram



6 MASS BALANCE (THEORETICAL)

The feedstocks for the process are vegetable oils and animal fats. NExBTL® Renewable Diesel plants are also able to process fatty acids such as PFAD (palm oil fatty acid distillate). Common triglyceride representations are shown below. The side chains R1, R2, R3 vary by length and are typically in the range of C14 to C18.

Figure 4 Triglyceride molecule models



A simplified mass balance for a model triglyceride $C_{57}H_{102}O_6$ (molecular weight 882 g/mole) is presented. Oxygen is removed as both water (H_2O) and as carbon dioxide (CO_2). The ratio depends on the catalyst and particular conditions employed. A typical ratio is shown in the example below. The equation is written without the production of bio-naphtha as only very small volumes of light hydrocarbons are formed.

A simplified mass balance of the renewable diesel process can be written as:



Since there are impurities removed in the pre-treatment of purification stage which must be removed prior to processing a slightly higher amount of feed is needed than in the above equation.

7 DESIGN CAPACITY

The Singapore plant has a design capacity of approximately 114 tonnes / hour NExBTL® renewable diesel. Based on an annual operating hours of 8760 hours this translates into 832 000 tonnes / year. During the period in question from September 1, 2011 to August 31, 2012 the plant was operating close to full capacity producing about 740 000 t of NExBTL®.

8 REALIZED SINGAPORE MASS BALANCE

The Singapore plant has been operating for approximately 2 years. The plant was officially opened in March 2011. During the start-up period, the plant capacity was raised and individual process units thoroughly tested. The results of energy and mass balances during the start-up phase of a production plant are not relevant for use in GHG calculations as the plant is not operating in a steady state mode and the energy consumption and chemicals consumption are not representative of full capacity values.

The mass balance for the period of September 1, 2011 to August 31, 2012 is shown in the table below. Comparison of the realized mass balance to that calculated from reaction stoichiometry in section 3 it can be seen that the actual values are very similar to the calculated values. Combining the values of HP & LP off gases (containing bio propane) gives 0.06 t/t NExBTL.

The carbon dioxide and water amounts are not reported in the table.

Table 3 Mass Balance NExBTL® Singapore 01.09.2011 - 31.08.2012

	t per t NExBTL®
Pretreatment Total Feed	1.21
NExBTL® Unit Feed	1.18
Hydrogen to NExBTL® Unit	0.038
NExBTL® Unit Production and Yields	
NExBTL® Product	1
Bio naphtha Product	0.0052
HP propane rich off gas	0.0505
LP propane rich off gas	0.0096

9 FEEDSTOCK PRE-TREATMENT SECTION

The function of the pre-treatment unit (PTU) is to reduce the level of impurities in the feed to acceptable levels and thus ensure a long catalyst lifetime.

The pre-treatment unit is designed for the continuously processing of vegetable oils and fats. The pre-treatment process is based on a bleaching unit (BLU). The bleaching unit can be operated independently from the rest of the plant and the operational configuration depends on the type and quality of the feedstock to be treated.

The bleaching process begins with the addition of an acid, forming a salt and removal of the salt by precipitation. The resultant feedstock is then fed through silica and/or bleaching earth which act as adsorbents for further reduction of impurities. Spent bleaching earth is disposed off-site.

The levels of acids or bleaching earth used are in the range of 0.003 to 0.0003 kg /kg of NExBTL® Renewable Diesel.

10 HYDRO TREATING SECTION

10.1 Hydro deoxygenation (HDO)

The catalytic hydro treatment of triglycerides occurs through consecutive reactions forming three, straight chain paraffins; plus propane, water and carbon dioxide with the amounts described earlier. There is 100% conversion of triglycerides in the reactor. This reaction step is normally referred to as hydro deoxygenation or HDO.

The reaction takes place by contacting the triglycerides with hydrogen over catalysts at elevated temperatures and pressures.

The HDO hydro treating reactions are exothermic. The excess heat that is produced must be removed from the process. This excess heat is used to heat up the incoming feed. This reduces the requirement for external energy.

The gases produced during this step are fed to the Recycle section after water has been condensed out for recycle and reuse.

10.2 Isomerization

After the HDO step, the paraffins are branched or isomerized. Isomerization is used to improve the cold flow properties of the final fuel. The reaction is carried out in an atmosphere of hydrogen but there is negligible hydrogen consumption in this step

The liquid hydrocarbons are next fed to the diesel stabilization column.

11 HYDROGEN PRODUCTION SECTION

Hydrogen is produced off-site in a Steam Methane Reformer (SMR). The SMR plant is located on nearby Jurong Island and connected to the Neste Oil Singapore plant via a hydrogen pipeline network. Hydrogen consumption was approximately 0.1 MJ / MJ_{NExBTL}.

Both natural gas and propane rich HP off gas are used in the SMR plant. The HP propane rich off gas is supplied in a dedicated pipeline. The natural gas used in the SMR plant is from the local natural gas network that is imported from Malaysia and Indonesia.

12 STABILIZATION SECTION

Product from the isomerization reactor is routed to the stabilization column where light hydrocarbons are separated by stripping with low pressure steam. The stripping steam is generated in the waste heat boiler from condensate with heat of the diesel stabilization column bottom product. Hydrocarbons that are stripped are called LP off gas.

13 GAS SEPARATION AND RECYCLE SECTION

The function of this section is to separate the gas mixture into individual gas streams for use or removal and disposal. Hydrogen is returned to the process for use while the high pressure (HP) propane rich off gas is sent to a steam methane reformer (SMR) for hydrogen production and low pressure (LP) propane rich off gas is sent to a natural gas steam boiler for process steam production.

The gases are selectively and sequentially removed by first absorption or washing with an aqueous amine solution followed by amine regeneration where the individual gases are separated.

The recycle section is comprised of a number of wash columns and regeneration columns. The carbon dioxide and water streams are cleaned before releasing to the atmosphere or to the wastewater system.

Hydrogen is recovered by its selective permeation through a membrane. Hydrogen is then compressed and ready for use in the process.

14 CO-PRODUCT HP PROPANE OFF GAS CREDIT

In the recycle section of the Neste Oil Oyj Singapore plant, the biogenic propane rich HP off gas generated by the process displaces an energy equivalent of natural gas (NG) that would otherwise have been consumed as both process fuel and as feedstock in the SMR. In order to calculate the greenhouse gas savings due to this HP propane rich off gas stream, this may be modelled by first assuming a NG only consumption in the SMR, that is without recycling of the off gas, and then subtracting a credit for the amount of NG displaced.

Based on the production figures for the Singapore plant during the time period in question, the propane rich HP off gas value had a GHG credit value of 3256.85 g CO₂e/MMBtu NExBTL and further to 3.09 g CO₂e/MJ NExBTL.

15 STEAM CONSUMPTION & PRODUCTION

The Neste Oil Singapore plant is located in the Tuas industrial area which is adjacent to the Tuas power plant. The process steam used in the Neste Oil NExBTL® Singapore plant is produced in a natural gas boiler in the Tuas Power Plant and utilizes natural gas is from the natural gas network and the low pressure (LP) propane rich off gas is from the NExBTL Singapore plant. As the propane rich off gas is biogenic, only the natural gas contributes to net greenhouse gas emissions.

16 POWER CONSUMPTION

During the period from September 1, 2011 to June 31, 2013, electrical power consumption in the Neste Oil Singapore NExBTL® plant was 163.58 BTU/lb NExBTL. This was purchased from the Singapore grid.

17 NExBTL® PHYSICAL DELIVERY

NExBTL® is transported from the production plant to a storage tank via pipeline over a distance of less than 1 mile. NExBTL® is transported for loading from the storage tank to the vessel via another pipeline over a distance of less than 1 mile.

NExBTL® is then shipped from Singapore to California discharge ports via ocean-going vessels over an average distance of 7,677 miles. Upon arrival, NExBTL® is discharged from the vessel to the onshore storage tanks via pipeline.

18 PATHWAY CI SUMMARY

The final carbon Intensity of the proposed pathway is summarized in the table below:

	Carbon Intensity in gCO₂e/MJ
Fish Oil Production (By rendering)	14.52
Fish Oil Transport	1.15
Renewable Diesel Production	11.13
Renewable Diesel Transport and Distribution	5.98
Total WTT	32.78
Total TTW	0.78
Propane Rich Off-Gas Credit	-3.09
Total WTW	30.48