

**California Environmental Protection Agency  
AIR RESOURCES BOARD**

**Executive Order G-70-179**

**Certification of the Catlow ICVN-VI Vacuum Assist  
Phase II Vapor Recovery System**

WHEREAS, the California Air Resources Board ("the Board" or "CARB") has established, pursuant to California Health and Safety Code sections 39600, 39601 and 41954, certification procedures for systems designed for the control of gasoline vapor emissions during motor vehicle fueling operations (Phase II vapor recovery systems) in its "CP-201 Certification Procedure for Vapor Recovery Systems of Dispensing Facilities" (the "Certification Procedures") as last amended April 12, 1996, incorporated by reference into Title 17, California Code of Regulations, Section 94011;

WHEREAS, the Board has established, pursuant to California Health and Safety Code sections 39600, 39601 and 41954, test procedures for determining the compliance of Phase II vapor recovery systems with emission standards in its "Certification and Test Procedures for Vapor Recovery Systems," CP-201.1 through CP-201.6 ("the Test Procedures") as adopted April 12, 1996, incorporated by reference into Title 17, California Code of Regulations, Section 94011;

WHEREAS, Catlow Incorporated ("Catlow") requested certification of the Catlow ICVN-VI bootless nozzle vapor recovery system (the "ICVN-VI system")

WHEREAS, the ICVN-VI system has been evaluated pursuant to the Board's Certification Procedures;

WHEREAS, the Certification Procedures (CP-201) provides that the Executive Officer shall issue an order of certification if he or she determines that the vapor recovery system conforms to all of the applicable requirements set forth in the Certification Procedures;

WHEREAS, I, Michael P. Kenny, Air Resources Board Executive Officer, find that the ICVN-VI system conforms with all the requirements set forth in the Certification Procedures, and results in a vapor recovery system which is at least 95 percent effective for attendant and/or self-serve use at gasoline service stations when used in conjunction with a Phase I vapor recovery system which has been certified by the Board and meets the requirements contained in Exhibit 2 of this Order.

NOW, THEREFORE, IT IS HEREBY ORDERED that the ICVN-VI system when used with a CARB-certified Phase I system, as specified in Exhibits 1 and 2 of this Order, is certified to be at least 95 percent effective in attended and/or self-serve mode. **Compatibility of this system with the onboard vapor recovery systems ("ORVR") has not been evaluated to determine the emissions impact. Fugitive emissions which may occur when the underground storage tanks are under positive pressure have not been quantified and were not included in the calculation of system effectiveness.** Exhibit 1 contains a list of

the equipment certified for use with the Catlow ICVN-VI system. Exhibit 2 contains installation and performance specifications for the system. Exhibit 3 contains a procedure for testing the static pressure integrity of the underground storage tank. Exhibit 4 contains a procedure for verifying dispensing rate.

IT IS FURTHER ORDERED that the dispensing rate for installations of the ICVN-VI system shall not exceed ten (10.0) gallons per minute when only one nozzle associated with the product supply pump is operating. This is consistent with the flowrate limitation imposed by United States Environmental Protection Agency as specified in the Federal Register, Volume 58, Number 55, page 16019. Dispensing rate shall be verified as specified in Exhibit 4.

IT IS FURTHER ORDERED that compliance with the certification requirements and rules and regulations of the Division of Measurement Standards of the Department of Food and Agriculture, the State Fire Marshal's Office, and the Division of Occupational Safety and Health of the Department of Industrial Relations is made a condition of this certification.

IT IS FURTHER ORDERED that the following requirements are made a condition of certification. The ICVN-VI system shall be installed only in facilities which are capable of demonstrating on-going compliance with the vapor integrity requirements contained in Exhibit 3 of this Order. The owner or operator of the installation shall conduct, and pass, a Static Pressure Decay test as specified in Exhibit 3, no later than 60 days after startup and at least once in each twelve month period. The owner or operator of the installation shall conduct, and pass, an Air-to-Liquid Ratio test as specified in TP-201.5 no later than 60 days after startup and at least once in each twelve month period thereafter. The test results shall be made available to the local air pollution control or air quality management district upon request within fifteen days after the tests are conducted, or within fifteen days of the request. Alternative test procedures may be used if determined by the Executive Officer, in writing, to yield comparable results.

IT IS FURTHER ORDERED that the ICVN-VI system, as installed, shall comply with the procedures and performance standards the test installation was required to meet during certification testing. If, in the judgment of the Executive Officer, a significant fraction of installations fail to meet the specifications of this certification, or if a significant portion of the vehicle population is found to have configurations which significantly impair the system's collection efficiency, the certification itself may be subject to modification, suspension or revocation.

IT IS FURTHER ORDERED that the certified ICVN-VI system shall, at a minimum, be operated in accordance with the manufacturer's recommended maintenance intervals and shall use the manufacturer's recommended operation, installation, and maintenance procedures.

IT IS FURTHER ORDERED that all nozzles approved for use with the ICVN-VI system shall be 100 percent performance checked at the factory, including checks of the integrity of the vapor and liquid path, as specified in Exhibit 2 of this Order, and of the proper functioning of all automatic shut-off mechanisms.

IT IS FURTHER ORDERED that each vapor pump shall be adjusted and 100 percent performance checked at the factory, including verification that the pump performance is within the range specified in Exhibit 2 of this Order.

IT IS FURTHER ORDERED that each vapor pump shall be adjusted and 100 percent performance checked at the factory, including verification that the pump performance is within the range specified in Exhibit 2 of this Order.

IT IS FURTHER ORDERED that the certified ICVN-VI system shall be performance tested during installation for ability to dispense gasoline and collect vapors without difficulty, in the presence of the station manager or other responsible individual. Catlow shall provide CARB-approved manuals to the station manager, owner or operator shall also be provided with instructions in the proper use of the ICVN-VI system, its repair and maintenance, where system and/or component replacements can be readily obtained, and shall be provided with copies of the installation and maintenance manuals for the ICVN-VI system to be maintained at the station. Revisions to the manual are subject to approval by CARB.

IT IS FURTHER ORDERED that the certified ICVN-VI system shall be warranted by Catlow, in writing, for at least one year, to the ultimate purchaser and each subsequent purchaser, that the vapor recovery system is designed, built and equipped so as to conform at the time of original installation or sale with the applicable regulations and is free from defects in materials and workmanship which would cause the vapor recovery system to fail to conform with applicable regulations. Catlow shall provide copies of the manufacturer's warranty and the operating and maintenance manuals for the Catlow ICVN-VI system to the station manager, owner or operator. Hoses, nozzles and breakaway couplings shall be warranted to the ultimate purchaser as specified above for at least one year, or for the expected useful life, whichever is longer.

IT IS FURTHER ORDERED that any alteration of the equipment, parts, design, or operation of the systems certified hereby is prohibited, and deemed inconsistent with this certification, unless such alteration has been approved by the Executive Officer or his/her designee.

Executed at Sacramento, California, this 2 day of JULY, 1997.

  
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Michael P. Kenny  
Executive Officer

Attachments

## Executive Order G-70-179

### Exhibit 1

#### Catlow ICVN-VI System Equipment List

<u>Component</u>	<u>Manufacturer/Model</u>	<u>State Fire Marshal Identification Number</u>
<b>Nozzles</b>	Catlow ICVN (Figure 1A) with vapor valve and ECD*	005:030:014
	Richards Astrovac (Figure 1B) with vapor valve and ECD*	005:031:018
	<u>OR</u> - Any bootless nozzle which has been CARB certified for use with the ICVN-VI system.	
	* ECD: Efficiency Compliance Device	
<b>Inverted Coaxial Hoses</b>	Catlow Vapor Mate	005:033:005
	Dayco 7282 Superflex 2000	005:033:005
	Dayco 7292 Superflex 4000	005:033:006
	Dayco 7246 Flex-Ever Ultimate	005:033:007
	Goodyear Flexsteel	005:036:002
	GT Sales/Hewitt Superflex 2000	005:033:005
	Thermoid Hi-Vac	005:037:003
	Thermoid Hi-Vac S	005:037:004
	VST VSTalflex	005:052:001
	VST VST-CIS	005:052:001
	<u>OR</u> - Any inverted coaxial hose CARB-certified for use with the ICVN-VI system.	
<b>Breakaway Couplings</b>	Catlow AV2001	005:030:006
	Catlow AVR200S	005:030:010
	Emco Wheaton A5219-001	005:030:010
	Husky 4034	005:021:009
	OPW 66CIP	005:030:006
	OPW 66FLB (w/ Flow Limiter)	005:008:055
	OPW 66CAS	005:008:056
	Richards Industries	
	VA-50	005:031:007
	VA-50B	005:031:014
	VA-60	005:031:009
STVA (w/ Swivel)	005:031:016	
	<u>OR</u> - Any inverted coaxial breakaway with a vapor valve which is CARB-certified for use with the ICVN-VI system.	

<u>Component</u>	<u>Manufacturer/Model</u>	<u>State Fire Marshal Identification Number</u>
<b>Swivels</b>	Richards MFVA	005:031:015
	<u>OR</u> – Any inverted coaxial swivel which is CARB-certified for use with the ICVN-VI system.	
<b>Flow Control Units</b>	Catlow I10G-1A	005:030:013
	Husky 5837	005:021:012
	OPW 66FL	005:008:054
	OPW 66FD	005:008:054
	Richards FRVAD	005:031:017
	Vapor Systems Technologies (VST)	005:044:001
	<u>OR</u> – Any inverted coaxial flow control unit which is CARB-certified for use with the ICVN-VI system.	
<b>Vapor Pumps</b>	Blackmer hydraulically driven vapor pump with a rotary vane motor. Model Number: VRFC	005:008:053
<b>Pressure/Vacuum Valve</b>	OPW 523LP, 523LPS (settings as specified below)	005:008:051
	Hazlett H-PVB-1 Gold label (settings as specified below)	005:017:004
	Morrison Brothers 749CRB0600 AV (settings as specified below)	005:041:001
	Morrison Brothers 749CRBS0600 AV (settings as specified below)	005:041:001
	<u>OR</u> – Any CARB-certified valve with the following pressure and vacuum settings, in inches water column (wc): <i>Pressure</i> : three plus or minus one-half inches (3.0 ± 0.5") water column. <i>Vacuum</i> : eight plus or minus two inches (8 ± 2") water column.	
<b>Phase I Product Adaptors</b>	Any CARB-certified rotatable Phase I product adaptor such as the OPW 61SA.	

**NOTE:** For systems installed before two CARB-certified rotatable Phase I product adaptors are available, or within sixty days after that date, any standard Phase I product adaptor may be used for a period not to exceed four years from the date the second rotatable Phase I product adaptor was certified.

## Executive Order G-70-179

### Exhibit 2

#### Specifications for the ICVN-VI Bootless Nozzle System

Figure 2A depicts the vapor pump mounting for the ICVN-VI system with different dispenser configurations. Proper positioning of the adapter for Air-to-Liquid testing is shown in Figure 2B. Figures 2C-1 through 2C-4 contain drawings of a typical installation of the ICVN-VI system.

#### Nozzles

1. An efficiency compliance device (ECD) shall be installed on the nozzle at the base of the spout, as shown in Figures 1A and 1B. Any nozzle with an ECD which is missing, or which is damaged such that at least three quarters (3/4) of the diameter is missing, or which has cumulative damage equivalent to at least 3/4 of the diameter missing, is defective and shall be immediately removed from service.
2. Failure mode testing demonstrated that blockage of some of the vapor collection holes in the spout has negligible effect on the operation of the system until only four holes remain unblocked. Any nozzle which is found to have less than four unobstructed vapor collection holes is defective and shall be immediately removed from service.
3. The ICVN and Astrovac nozzles each have an integral vapor valve which prevents the loss of vapor from the underground storage tanks and ensures proper operation of the system. Any nozzle with a defective vapor valve shall be immediately removed from service and the vapor path shall be closed as soon as practicable.
4. Nozzles shall be 100 percent performance checked at the factory, including checks of all shutoff mechanisms and of the integrity of the vapor path. The maximum allowable leak rate for the nozzle shall not exceed the following:  
  
0.038 CFH at a pressure of two inches water column (2" wc), and  
0.005 CFH at a vacuum of twenty seven inches water column (approx. 1 psi).
5. No sealing of the vapor holes on the nozzle spout (such as placing a balloon or the fingers of a glove over the holes) is permitted during static pressure decay tests.

#### Inverted Coaxial Hoses

1. The length of hose which may be in contact with the island and/or ground when the nozzle is properly mounted on the dispenser is limited to six inches (6").
2. Within the constraints of the accepted configuration, high or low hang, the maximum allowable length of the hose shall be fifteen feet (15').

### **Breakaway Couplings**

1. Breakaway couplings are optional but, if installed, only CARB-certified breakaways which close the vapor path may be used.

### **ICVN-VI System**

1. One Blackmer model VRFC pump shall be installed for each dispensing nozzle. Figure 2A provides an illustration for the typical mounting of the vapor pump with low and high hose hang dispenser configurations.
2. The pump shall be installed, at a minimum, in accordance with the instructions of the manufacturer. Any modification of the dispenser piping must be made in accordance with the instructions of the dispenser manufacturer.
3. The pump shall be serviced only by a qualified contractor. Field service of the pump is prohibited.
4. The pump makes an audible clicking sound when operating normally. The clicking sound may be masked by background noise.
5. The normal operating range of the system, as measured by air-to-liquid (A/L) ratio testing, is 1.02. plus or minus 0.10 (0.92 to 1.12). The A/L ratio shall be determined by the CARB-approved (TP-201.5) and shall be measured at a flowrate between six and ten gallons per minute (6 - 10 gpm). Alternative test procedures may be used if they are determined by the Executive Officer to yield comparable results. Any fueling point not capable of demonstrating compliance with this performance standard shall be deemed defective and removed from service.

The measurements shall be taken not including the nozzle aspirator port. It is recommended that the aspirator contribution be excluded because this volume is injected into the product stream and does not go through the vapor pump. Figure 2B illustrates the proper configuration of the A/L adapter.

NOTE: This test procedure returns air rather than vapor to the storage tank, and normally causes an increase in storage tank pressure which may result in vent emissions. This is a temporary condition due to the test and should not be considered an indication of malfunction or noncompliance.

### **Pressure/Vacuum Valves for Storage Tank Vents**

1. A pressure/vacuum (P/V) valve shall be installed on each tank vent. Vent lines may be manifolded to minimize the number of P/V valves and potential leak sources, provided the manifold is installed at a height not less than 12 feet above the driveway surface used for Phase I tank truck filling operations. At least one P/V valve shall be installed on manifolded vents. If two P/V valves are desired, they shall be installed in parallel, so that each can serve as a backup for the other if one should fail to open properly. The P/V valve shall be a CARB-certified valve as specified in Exhibit 1. The outlets shall vent upward and be located to eliminate the possibility of vapor accumulating or traveling to a source of ignition or entering adjacent buildings.

### **Vapor Recovery Piping Configurations**

1. The recommended maximum pressure drop through the system, measured at a flow rate of 60 SCFH with dry Nitrogen gas, is 0.02 inches water column (0.03 inches wc at 60 SCFH if the measurement includes an impact valve). The maximum allowable pressure drop through the system shall never exceed one-half inch (0.5") water column at 60 SCFH. The pressure drop shall be measured from the dispenser riser to the UST with the pressure/vacuum valves installed and with the poppeted Phase I vapor connection open.
2. All vapor return lines shall slope a minimum of 1/8 inch per foot. A slope of 1/4 inch or more per foot is recommended wherever feasible.
3. The dispenser shall be connected to the riser with either flexible or rigid material which is listed for use with gasoline. The dispenser-to-riser connection shall be installed so that any liquid in the lines will drain toward the storage tank. The internal diameter of the connector, including all fittings, shall not be less than three-fourths inch (3/4").
4. The recommended nominal inside diameter of the underground Phase II plumbing is as indicated in Figures 2C-1 through 2C-4. Smaller vapor lines are not recommended but may be used provided the pressure drop criteria specified above are met. The vapor return lines shall be manifolded as shown in Figures 2C-1 through 2C-4.

EXCEPTION: For installations with a vapor return line directly to only one tank, and for which a manifold on the tank vents will be used to provide part of the vapor return path to other tanks, the vent manifold may be used as an alternative to the underground manifold only in existing installations where the vapor piping is already installed, and shall not be used in "new" installations where vapor piping is being installed. For installations with dedicated vapor piping directly to each tank, the vent manifold is approved for both new and existing installations and an additional tank manifold below grade is optional but not required.

5. All vapor return and vent piping shall be installed in accordance with the manufacturer's instructions and all applicable regulations.

6. No product shall be dispensed from any fueling point associated with a vapor line which is disconnected and open to the atmosphere. If vapor lines are manifolded, this includes all fueling points in the facility.

### **Phase I System**

**WARNING:** Phase I fill caps should be opened with caution because the storage tank may be under pressure.

1. The Phase I system shall be a CARB-certified system which is in good working order and which demonstrates compliance with the static pressure decay test criteria contained in Exhibit 3 of this Order. Coaxial Phase I systems shall not be used with new installations of the system. Replacement of storage tanks at existing facilities, or modifications which cause the installation of new or replacement Phase I vapor recovery equipment, are considered new installations with regard to this prohibition. An exception to this prohibition may be made for coaxial Phase I systems CARB-certified after January 1, 1994, as compatible for use with Phase II systems which require pressure/vacuum vent valves.

Where installation of the Catlow ICVN-VI system is made by retrofitting previously installed equipment, local districts may elect to allow existing coaxial Phase I systems to remain in use for a specifically identified period of time provided the following conditions are met:

- the existing coaxial Phase I system is a poppeted, CARB-certified system capable of demonstrating compliance with the static pressure decay test as specified above when tested with the fill cap removed; and
  - installation of the Phase II system requires no modification of the UST(s) and/or connections.
2. Spill containment manholes which have drain valves shall demonstrate compliance with the static pressure decay criteria with the drain valves installed as in normal operation. Manholes with cover-actuated drain valves shall not be used in new installations (as defined above). Manholes with cover-actuated drain valves may remain in use in facilities where installation of the Catlow ICVN-VI system does not require modification of the tank fittings provided the facility demonstrates compliance with static pressure decay test criteria both with the cover open and with the cover closed.
  3. The Phase I vapor recovery system shall be operated during product deliveries so as to minimize the loss of vapors from the facility storage tank which may be under pressure. There shall be no less than one vapor return hose connected for each product being delivered. Provided it is not in conflict with established safety procedures, this may be accomplished in the following manner:
    - the Phase I vapor return hose is connected to the delivery tank and to the delivery elbow before the elbow is connected to the facility storage tank;
    - the delivery tank is opened only after all vapor connections have been made, and is closed before disconnection of any vapor return hoses;

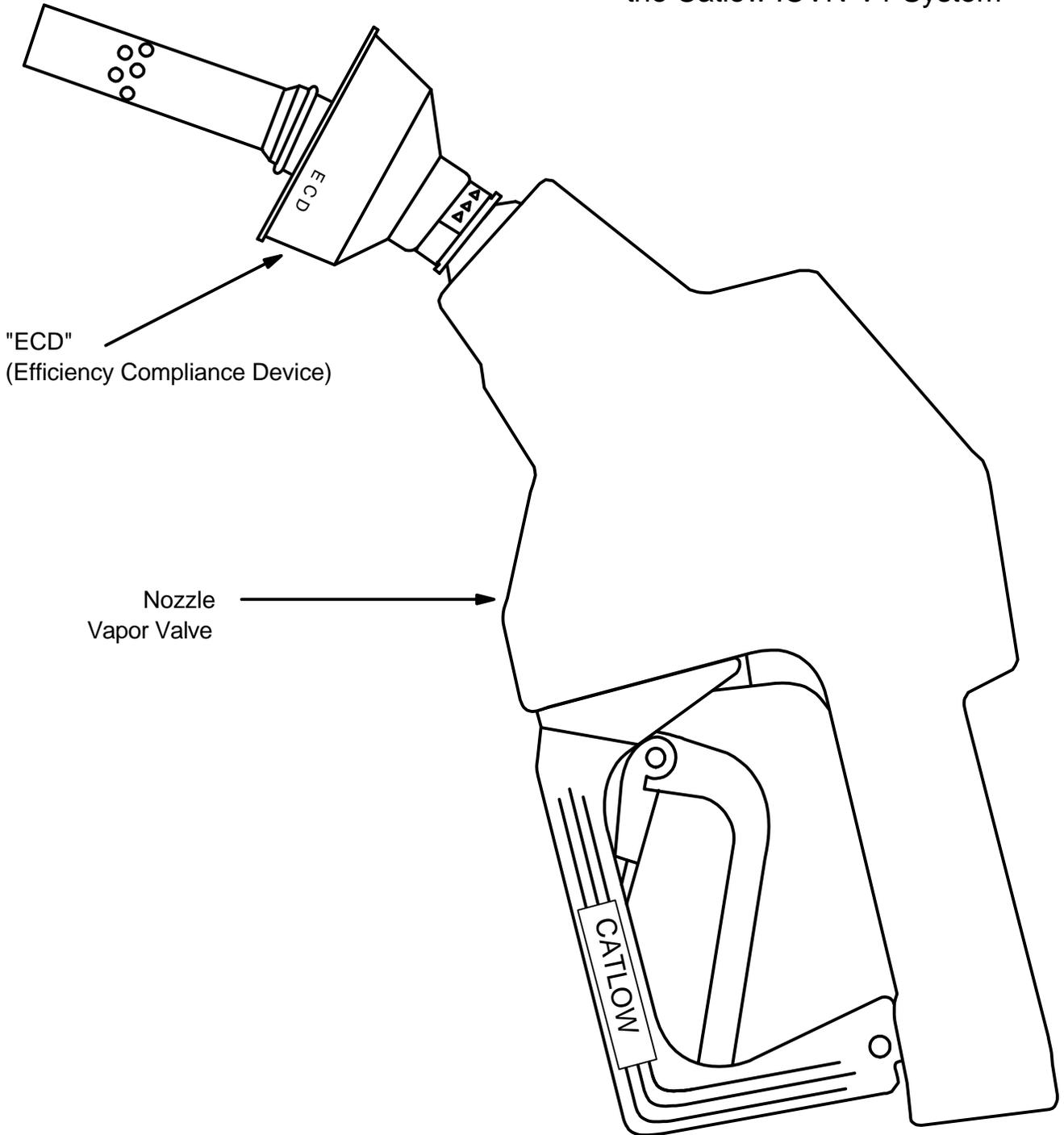
- the vapor return hose is disconnected from the facility storage tank before it is disconnected from the delivery tank.
4. Phase I deliveries shall be accomplished so as to ensure that there is at least one vapor connection between the cargo tank compartment headspace and the storage tank associated with the product delivery. There shall be no more than two product hoses used with one vapor hose connected, and no more than three product hoses used with two vapor hoses connected.
  5. Storage tank vent pipes, and fill and vapor and manhole tops, shall be maintained white, silver or beige. Colors which will similarly prevent heating of the system due to solar gain may also be used, provided they are listed in EPA AP-42 as having a factor the same as or better than that of the colors listed above. Existing facilities which were installed before April 1, 1996, must be in compliance with this requirement no later than January 1, 1998. Manhole covers which are color coded for product identification are exempted from this requirement.

**Executive Order G-70-179**

**Exhibit 1**

**Figure 1A**

Catlow ICVN Nozzle for  
the Catlow ICVN-V1 System

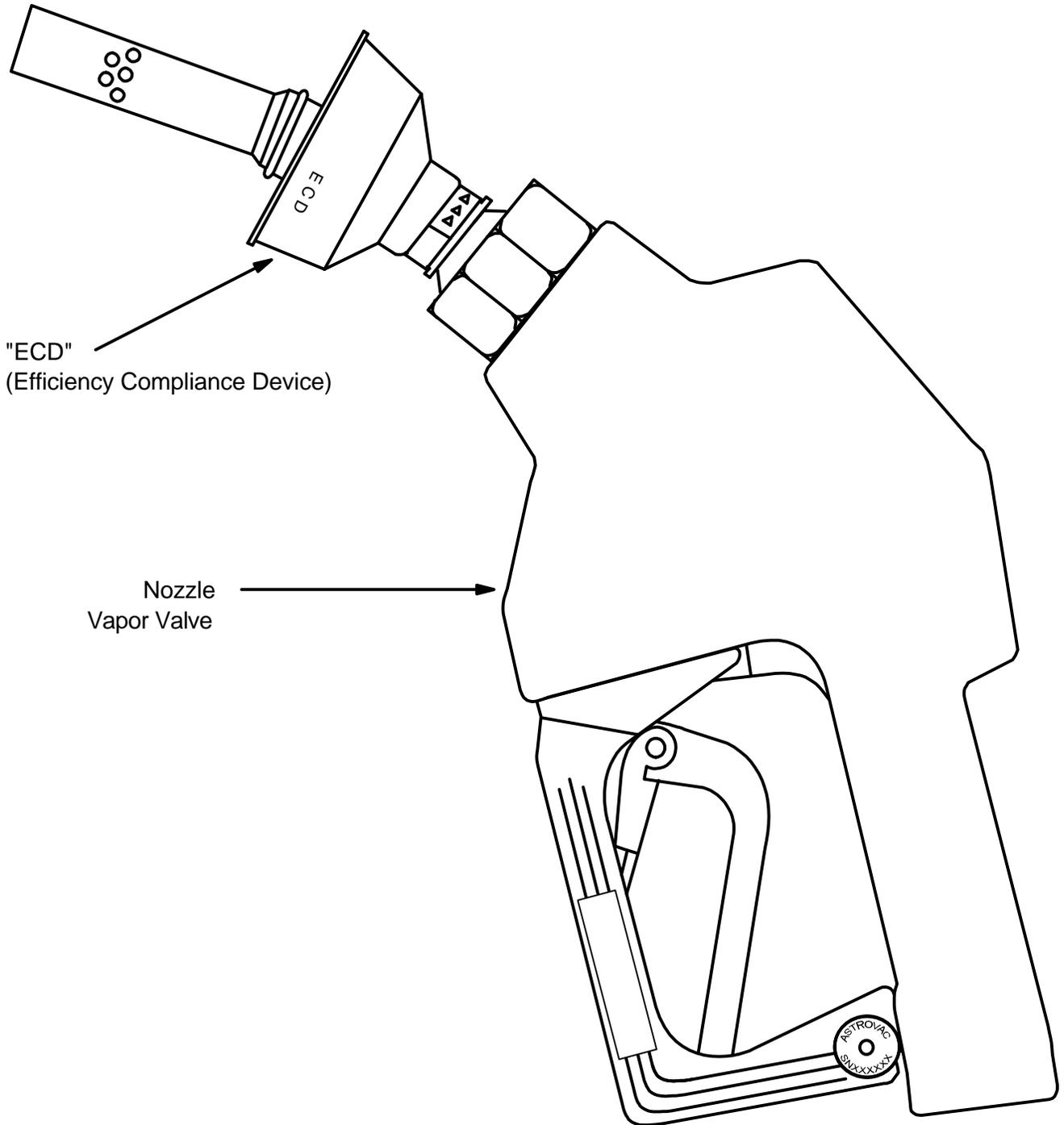


**Executive Order G-70-179**

**Exhibit 1**

**Figure 1-B**

Richards Astrovac Nozzle for  
the Catlow ICVN-V1 System



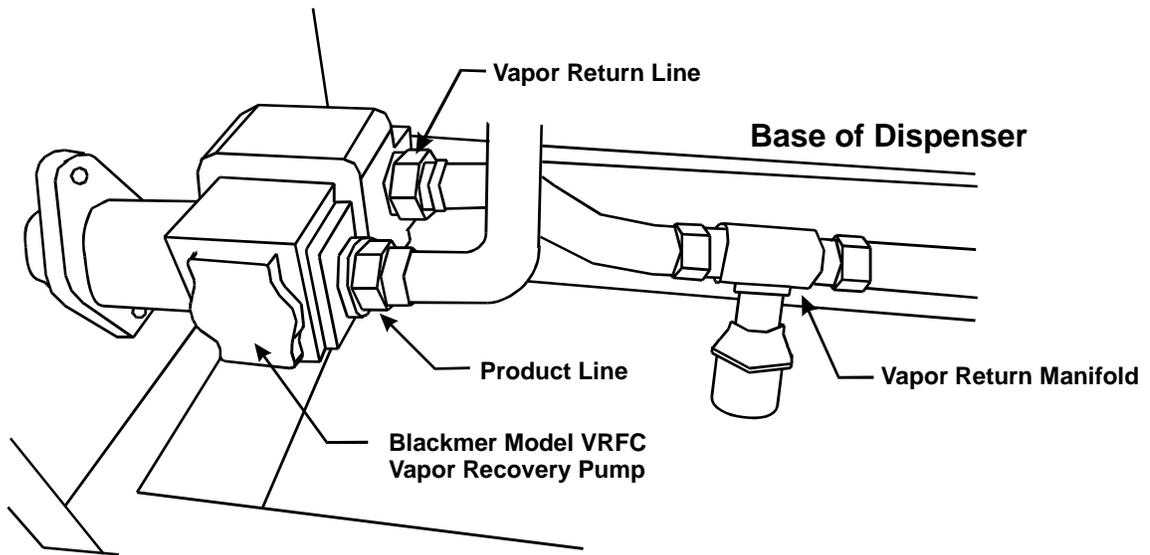
# Executive Order G-70-179

## Exhibit 2

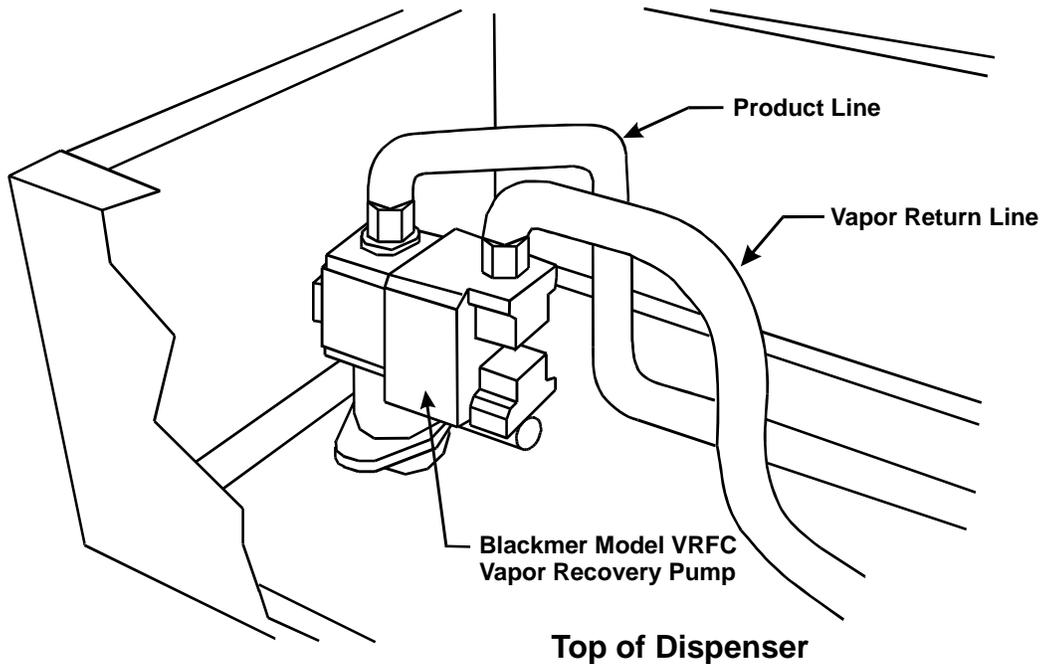
### Figure 2A

#### Typical Mounting of Vapor Pumps for Catlow ICVN-VI Phase II Vapor Recovery System

##### (i) Low Hose Hang Dispenser Configuration



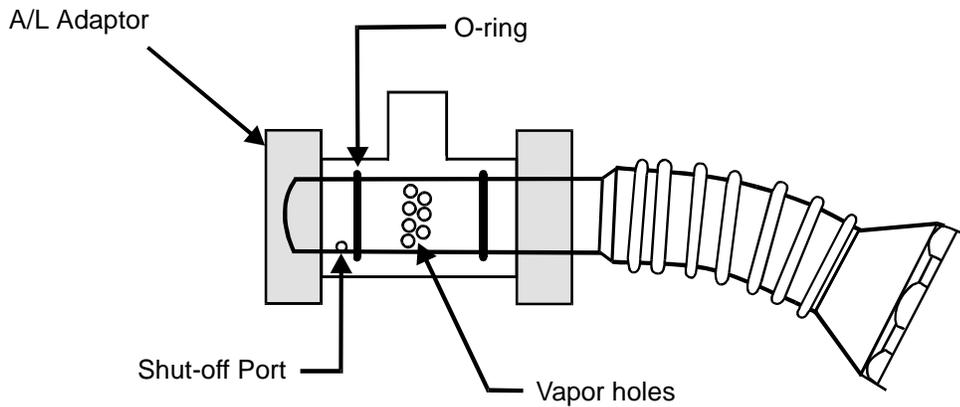
##### (ii) High Hose Hang Dispenser Configuration



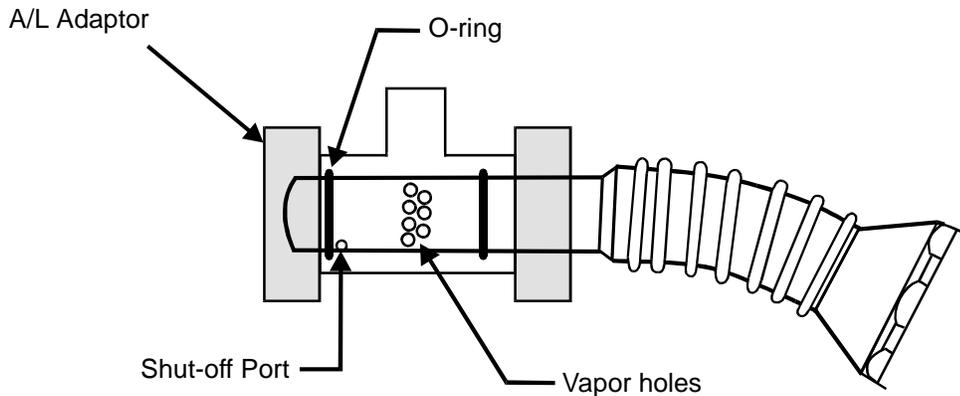
**Executive Order G-70-179**  
**Exhibit 2**  
**Figure 2B**

**Proper Installation of the A/L Adaptor**

**Correct Installation:** Note that the o-ring has isolated the shut-off port from the vapor holes



**Incorrect Installation:** Note that the o-ring includes the shut-off port with the vapor holes

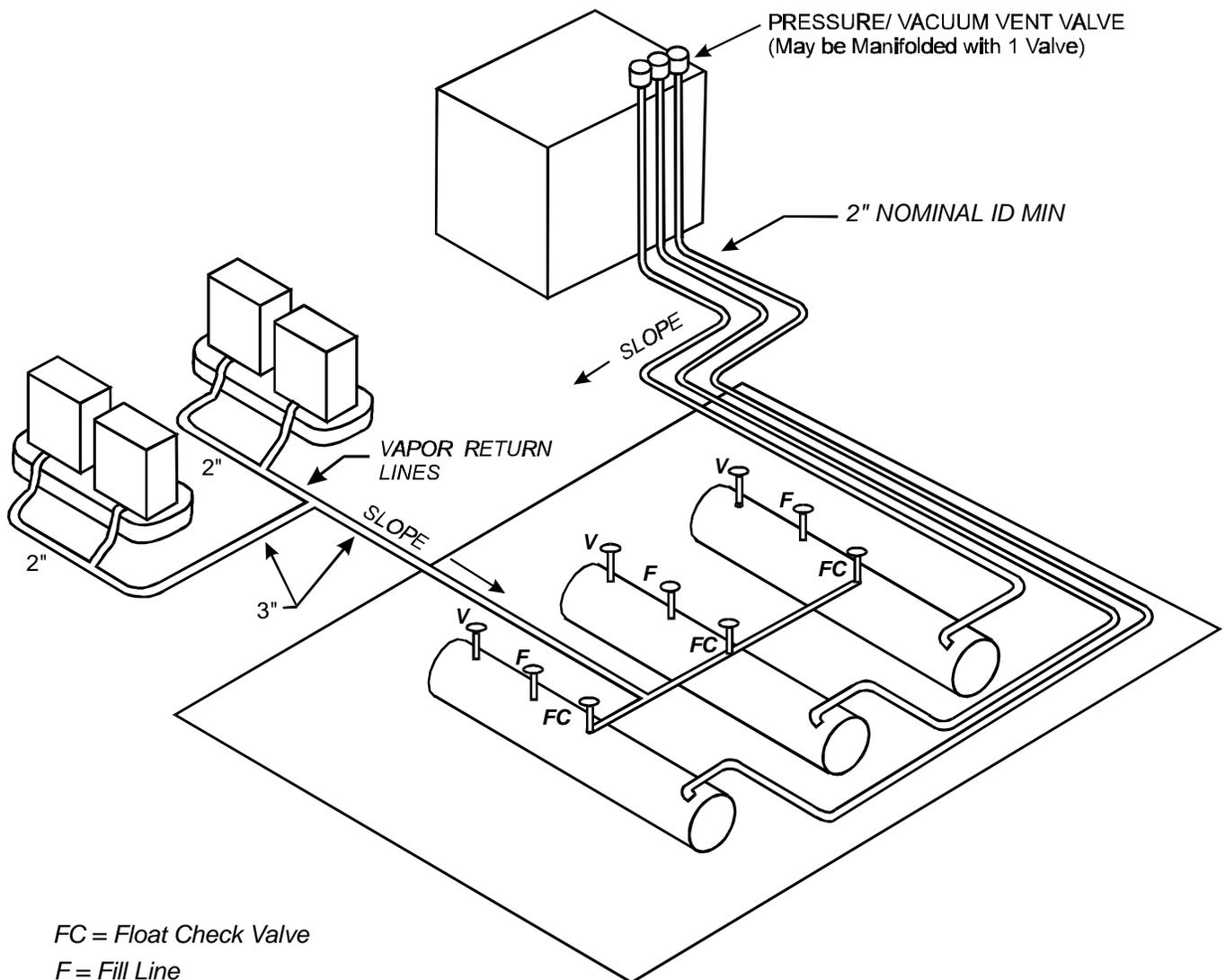


# Executive Order G-70-179

## Exhibit 2

### Figure 2C-1

Typical Installation of the  
Catlow ICVN-VI Phase II Vapor Recovery System  
with Two-Point Phase I System



FC = Float Check Valve

F = Fill Line

V = Phase I Vapor Recovery

Note: 1. All Vapor/Vent Lines are 3" Nominal ID Minimum Except as Noted

2. Slope: 1/8" per foot Min.

1/4" per Foot Preferred

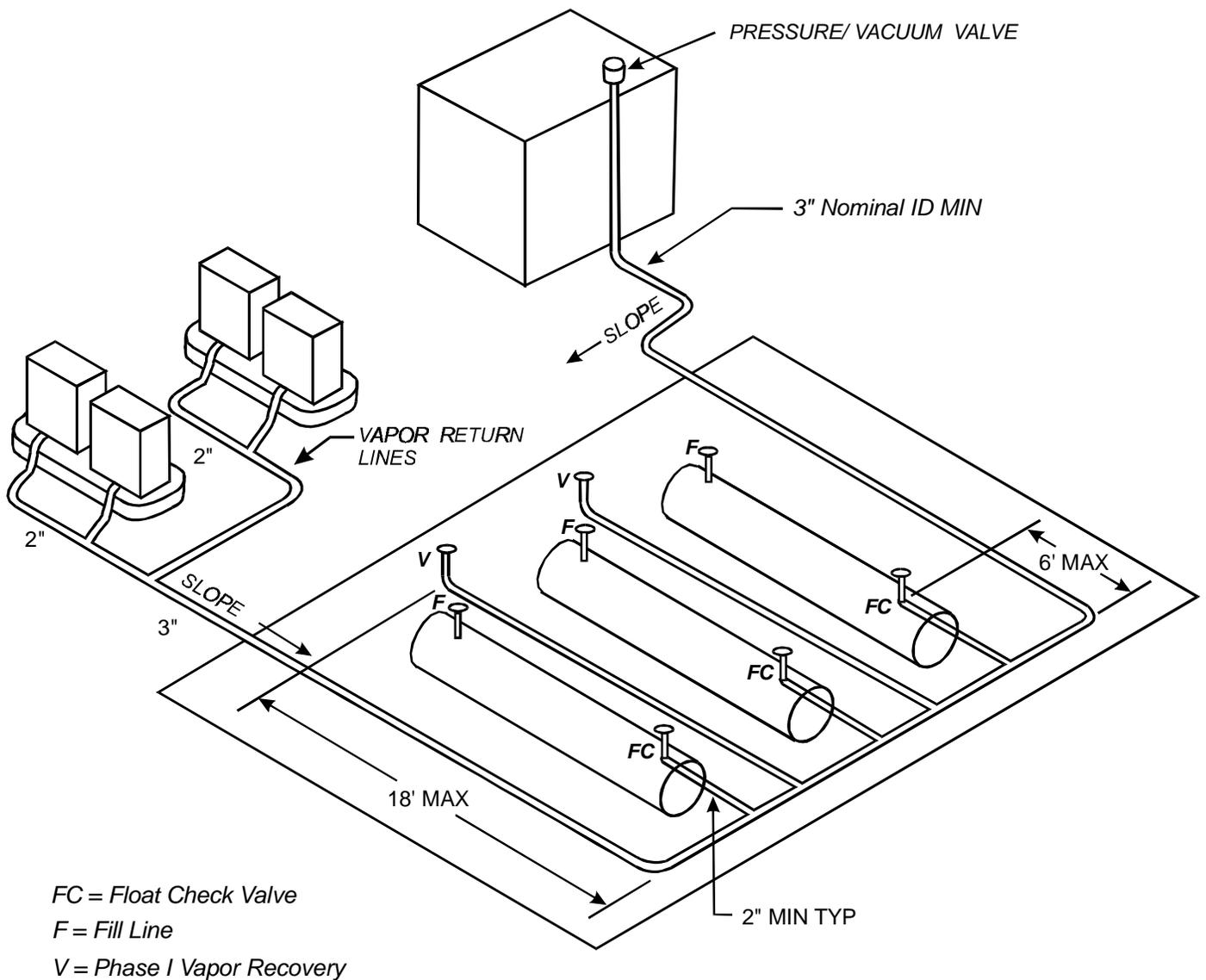
3. Maintain 2'0" Clearance Between Fill Line and  
Phase I Vapor Return Line to Delivery Truck

# Executive Order G-70-179

## Exhibit 2

### Figure 2C-2

Typical Installation of the  
Catlow ICVN-VI Phase II Vapor Recovery System  
with Two-Point Phase I System



Note: 1. All Vapor/Vent Lines are 3" Nominal ID Minimum Except as Noted

2. Slope: 1/8" per foot Min.

1/4" per Foot Preferred

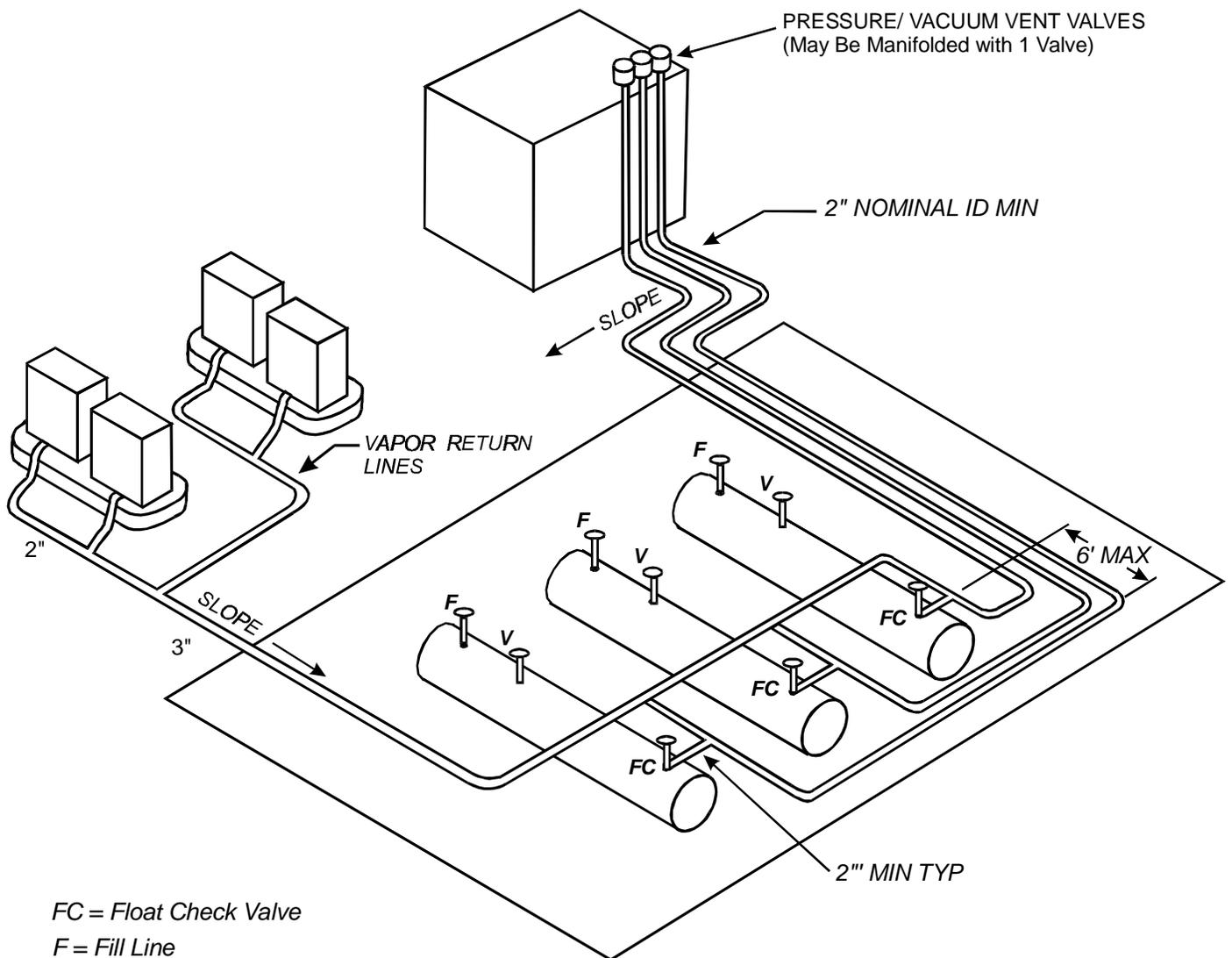
3. Maintain 2'0" Clearance Between Fill Line and  
Phase I Vapor Return Line to Delivery Truck

# Executive Order G-70-179

## Exhibit 2

### Figure 2C-3

#### Typical Installation of the Catlow ICVN-VI Phase II Vapor Recovery System with Two-Point Phase I System



FC = Float Check Valve

F = Fill Line

V = Phase I Vapor Recovery

Note: 1. All Vapor/Vent Lines are 3" Nominal ID Minimum Except as Noted

2. Slope: 1/8" per foot Min.

1/4" per Foot Preferred

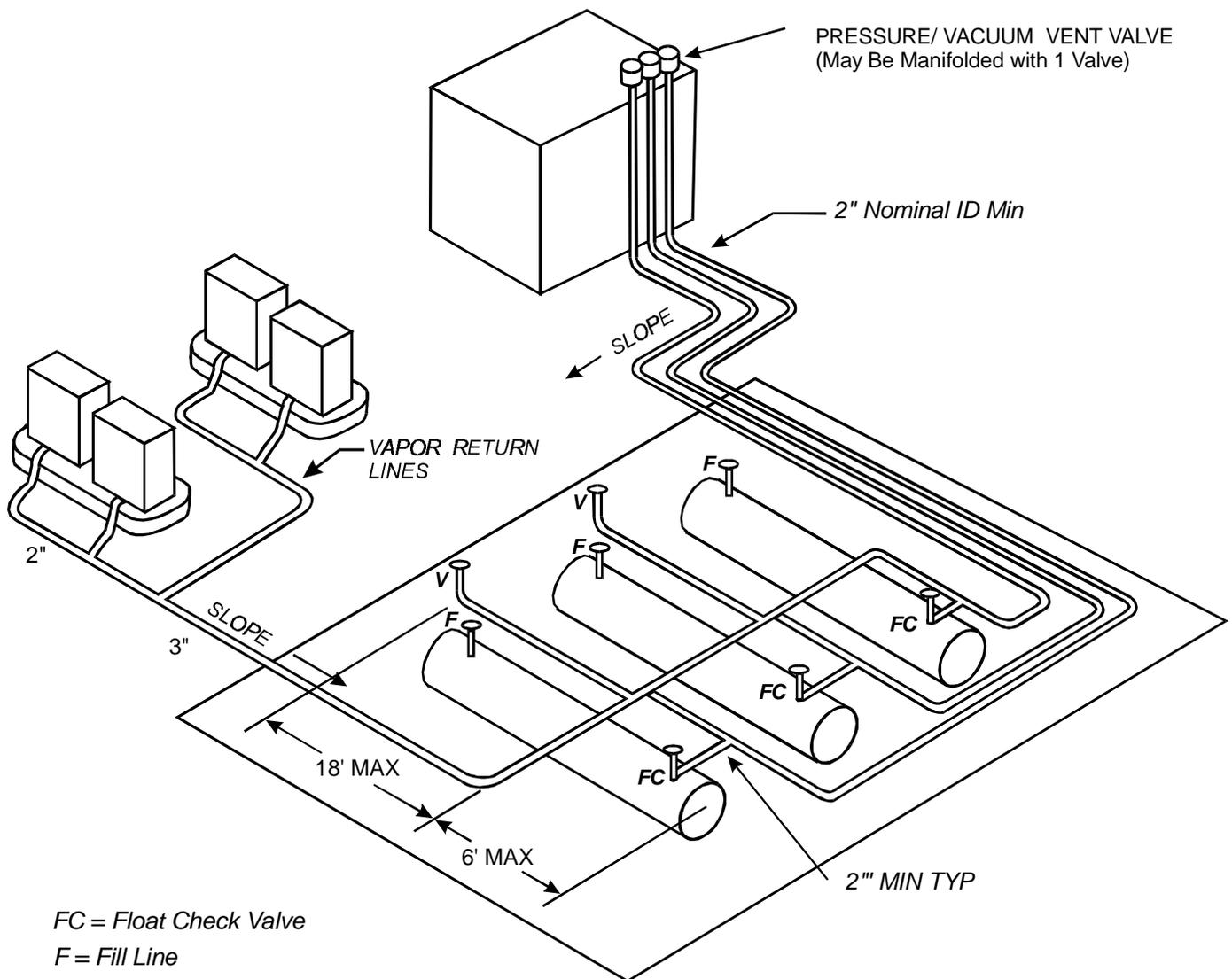
3. Maintain 2'0" Clearance Between Fill Line and  
Phase I Vapor Return Line to Delivery Truck

# Executive Order G-70-179

## Exhibit 2

### Figure 2C-4

#### Typical Installation of the Catlow ICVN-VI Phase II Vapor Recovery System with Two-Point Phase I System



FC = Float Check Valve

F = Fill Line

V = Phase I Vapor Recovery

Note: 1. All Vapor/Vent Lines are 3" Nominal ID Minimum Except as Noted

2. Slope: 1/8" per foot Min.

1/4" per Foot Preferred

3. Maintain 2'0" Clearance Between Fill Line and  
Phase I Vapor Return Line to Delivery Truck

# Executive Order G-70-179

## Exhibit 3

### STATIC PRESSURE INTEGRITY TEST UNDERGROUND STORAGE TANKS

#### 1. APPLICABILITY

- 1.1 This test procedure is used to quantify the vapor tightness of vapor recovery systems installed at gasoline dispensing facilities (GDF) equipped with vacuum assist systems which require pressure/vacuum (P/V) valves, provided that the designed pressure setting of the P/V valves is a minimum of 2.5 inches of water column (inches H<sub>2</sub>O). Excessive leaks in the vapor recovery system will increase the quantity of fugitive hydrocarbon emissions and lower the overall efficiencies of both the Phase I and Phase II vapor recovery systems.
- 1.2 Systems equipped with a P/V valve(s) allowed to have a designed cracking pressure less than 2.5 inches H<sub>2</sub>O shall be bagged to eliminate any flow contribution through the valve assembly from the test results. The valve/vent pipe connection, however, shall remain unobstructed during this test.

#### 2. PRINCIPLE

- 2.1 The entire vapor recovery system is pressurized with nitrogen to two (2.0) inches H<sub>2</sub>O. The system pressure is then allowed to decay and the pressure after five (5) minutes is compared with an allowable value. The minimum allowable five-minute final pressure is based on the system ullage and pressure decay equations. For the purpose of compliance determination, this test shall be conducted after all back-filling, paving, and installation of all Phase I and Phase II components, including P/V valves, has been completed.
- 2.2 For GDF equipped with a coaxial Phase I system, this test shall be conducted at a Phase II vapor riser. For GDF which utilize a two-point Phase I system, this test may be conducted at either a Phase II riser or a Phase I vapor coupler provided that the criteria set forth in Section 6.7 have been met. If the integrity criteria for two-point systems specified in Section 6.7 are met, it is recommended that this test be conducted at the Phase I vapor coupler.

#### 3. RANGE

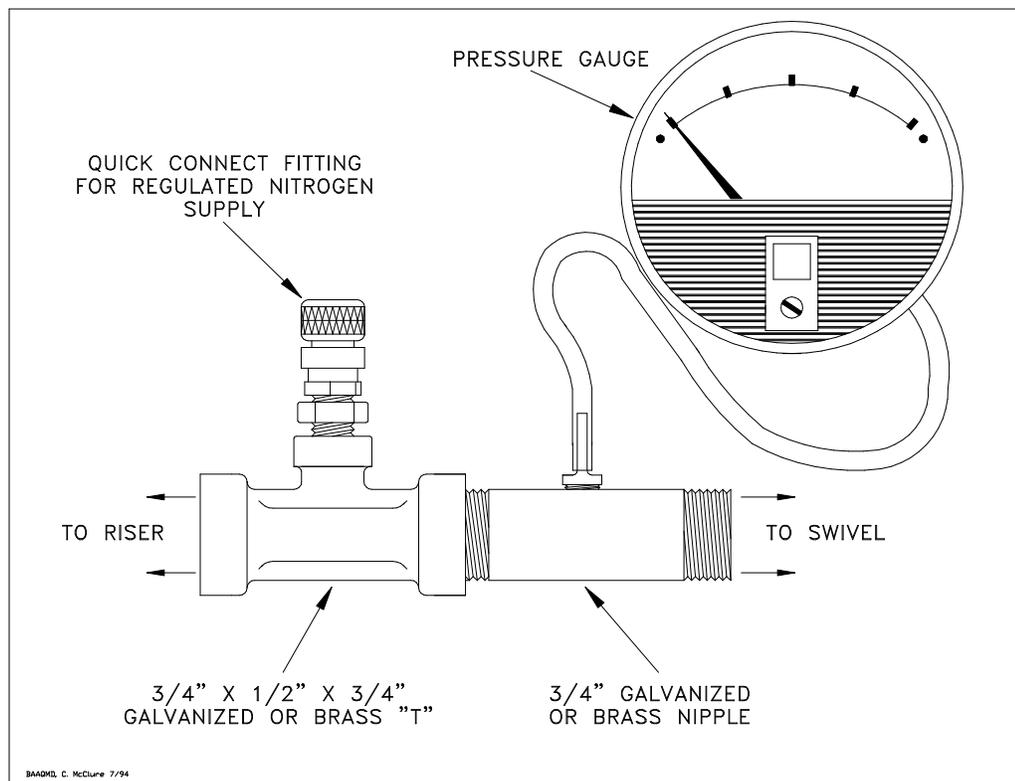
- 3.1 If mechanical pressure gauges are employed, the full-scale range of the pressure gauges shall be 0-2.0, 0-1.0, and 0-0.50 inches H<sub>2</sub>O column. Maximum incremental graduations of the pressure gauge shall be 0.05 inches H<sub>2</sub>O and the minimum accuracy of the gauge shall be three percent of full scale. The minimum diameter of the pressure gauge face shall be 4 inches. A 0-2 inches H<sub>2</sub>O inclined manometer, or equivalent, may be used provided that the minor scale divisions do not exceed 0.02 inches H<sub>2</sub>O.

- 3.2 If an electronic pressure measuring device is used, the full-scale range of the device shall not exceed 0-10 inches H<sub>2</sub>O with a minimum accuracy of 0.5 percent of full-scale. A 0-20 inches H<sub>2</sub>O device may be used, provided the equivalent accuracy is not less than 0.25 percent of full scale.
- 3.3 The minimum and maximum total ullages shall be 500 and 25,000 gallons, respectively. These values are exclusive of all vapor piping volumes.
- 3.4 The minimum and maximum nitrogen feed-rates, into the system, shall be one (1) and five (5) CFM, respectively.

#### 4. INTERFERENCES

- 4.1 Introduction of nitrogen into the system at flowrates exceeding five (5) CFM may bias the results of the test toward non-compliance. Only gaseous nitrogen shall be used to conduct this test. Air, liquified nitrogen, helium, or any gas other than nitrogen **shall not be used** for this test procedure.
- 4.2 The results of this Static Pressure Integrity Test shall not be used to verify compliance if an Air to Liquid Volumetric Ratio Test (Test Procedure TP-210.5 or equivalent) was conducted within the 24 hours prior to this test.

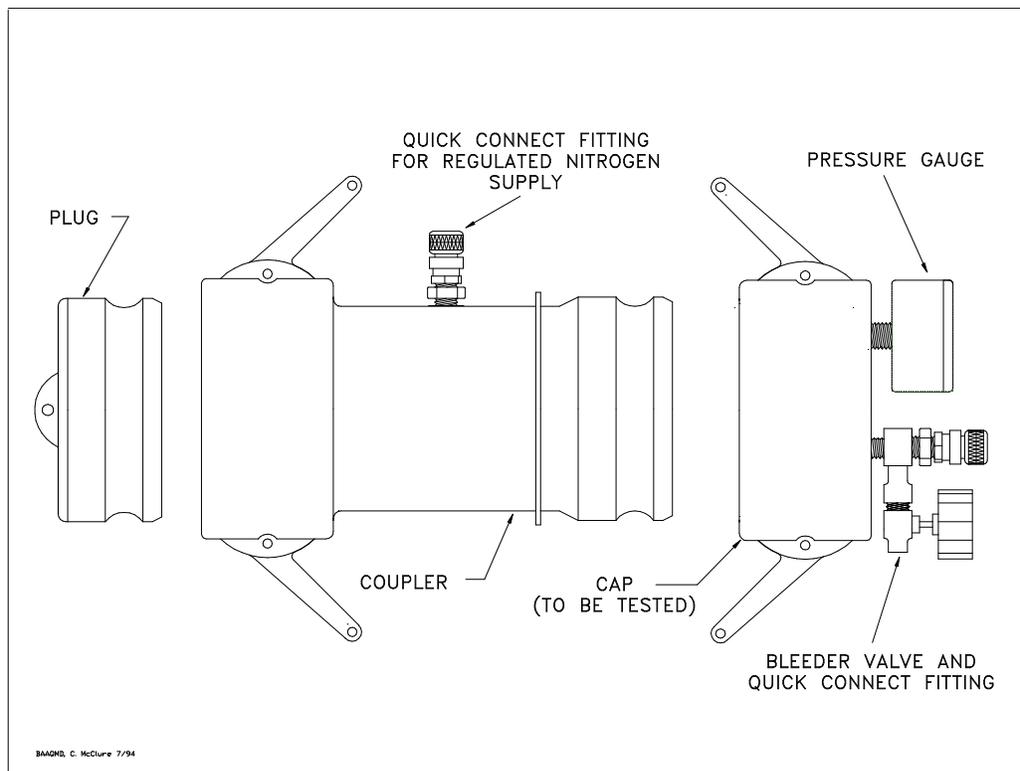
**Figure 3-1**  
**"T" Connector Assembly**



## 5. APPARATUS

- 5.1 Nitrogen. Use commercial grade nitrogen in a high pressure cylinder, equipped with a two-stage pressure regulator and a one psig pressure relief valve.
- 5.2 Pressure Measuring Device. Use 0-2.0, 0-1.0, and 0-0.50 inches H<sub>2</sub>O pressure gauges connected in parallel, a 0-2 inches H<sub>2</sub>O manometer, or an electronic pressure measuring device to monitor the pressure decay in the vapor recovery system. The pressure measuring device shall, at a minimum, be readable to the nearest 0.05 inches H<sub>2</sub>O.
- 5.3 "T" Connector Assembly. See Figure 3-1 for example.
- 5.4 Vapor Coupler Integrity Assembly. Assemble OPW 633-A, 633-B, and 634-A adapters, or equivalent, as shown in Figure 3-2. If the test is to be conducted at the storage tank Phase I vapor coupler, this assembly shall be used prior to conducting the static leak test in order to verify the pressure integrity of the vapor poppet. The internal volume of this assembly shall not exceed 0.1 cubic feet.

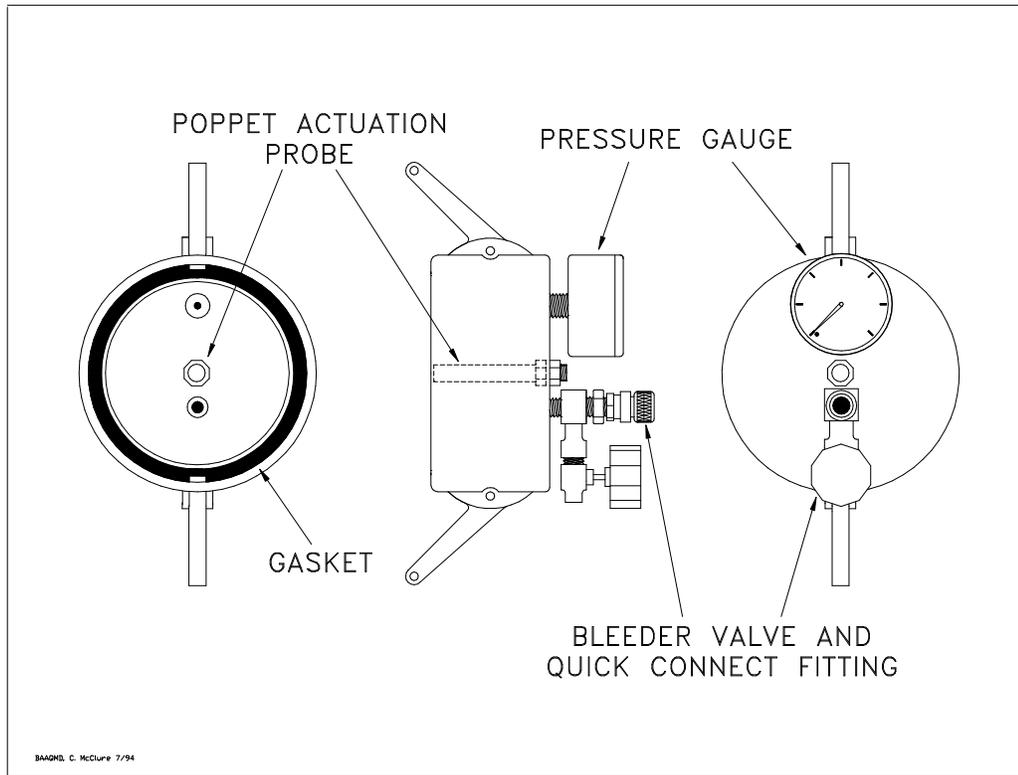
**Figure 3-2**  
**Vapor Coupler Integrity Assembly**



- 5.5 Vapor Coupler Test Assembly. Use a compatible OPW 634-B cap, or equivalent, equipped with a center probe to open the poppet, a pressure

measuring device to monitor the pressure decay, and a connection for the introduction of nitrogen into the system. See Figure 3-3 for an example.

**Figure 3-3**  
**Vapor Coupler Test Assembly**



- 5.6** Stopwatch. Use a stopwatch accurate to within 0.2 seconds.
- 5.7** Flowmeter. Use a Dwyer flowmeter, Model RMC-104, or equivalent, to determine the required pressure setting of the delivery pressure gauge on the nitrogen supply pressure regulator. This pressure shall be set such that the nitrogen flowrate is between 1.0 and 5.0 CFM.
- 5.8** Combustible Gas Detector. A Bacharach Instrument Company, Model 0023-7356, or equivalent, may be used to verify the pressure integrity of system components during this test.
- 5.9** Leak Detection Solution. Any liquid solution designed to detect vapor leaks may be used to verify the pressure integrity of system components during this test.

## 6. PRE-TEST PROCEDURES

- 6.1** The following safety precautions shall be followed:
  - 6.1.1** Only nitrogen shall be used to pressurize the system.
  - 6.1.2** A one psig relief valve shall be installed to prevent the possible over-pressurizing of the storage tank.
  - 6.1.3** A ground strap should be employed during the introduction of nitrogen into the system.
- 6.2** Failure to adhere to any or all of the following time and activity restrictions shall invalidate the test results:
  - 6.2.1** There shall be no Phase I bulk product deliveries into or out of the storage tank(s) within the three (3) hours prior to the test or during performance of this test procedure .
  - 6.2.2** There shall be no product dispensing within thirty (30) minutes prior to the test or during performance of this test procedure.
  - 6.2.3** Upon commencement of the thirty minute “no dispensing” portion of this procedure, the headspace pressure in the tank shall be measured. If the pressure exceeds 0.50 inches H<sub>2</sub>O, the pressure shall be carefully relieved in accordance with all applicable safety requirements. After the thirty minute “no dispensing” portion of this procedure, and prior to introduction of nitrogen, the headspace pressure shall again be lowered, if necessary, to less than 0.50 inches H<sub>2</sub>O.
  - 6.2.4** There shall be no Air to Liquid Volumetric Ratio Test (Test Procedure TP-201.5) conducted within the twenty-four (24) hour period immediately prior to this test.
- 6.3** Measure the gallons of gasoline present in each underground storage tank and determine the actual capacity of each storage tank from facility records. Calculate the ullage space for each tank by subtracting the gasoline gallonage present from the actual tank capacity. The minimum ullage during the test shall be 25 percent of the tank capacity or 500 gallons, whichever is greater. The total ullage shall not exceed 25,000 gallons.
- 6.4** For two-point Phase I systems, this test shall be conducted with the dust cap removed from the vapor coupler. This is necessary to determine the vapor tightness of the Phase I vapor poppet. See Section 6.7 if this test is to be conducted at the Phase I vapor coupler.
  - 6.4.1** For coaxial Phase I systems, this test shall be conducted with the dust cap removed from the Phase I coupler. This is necessary to insure the vapor tightness of the Phase I vapor poppet.
  - 6.4.2** Verify that the liquid level in the storage tank is at least four (4) inches above the highest opening at the bottom of the submerged drop tube.
- 6.5** If the Phase I containment box is equipped with a drain valve, the valve assembly may be cleaned and lubricated prior to the test. This test shall,

however, be conducted with the drain valve installed and the manhole cover removed. See subsection 7.4.1 for further details regarding containment box drain valves.

**6.6** If the test is to be conducted at a Phase II vapor riser, disconnect the dispenser end of one vapor recovery hose and install the "T" connector assembly (see Figure 3-1). Connect the nitrogen gas supply (do not use air) and the pressure measuring device to the "T" connector.

**6.6.1** For those Phase II systems utilizing a dispenser mounted remote vapor check valve, the "T" connector assembly shall be installed on the vapor riser side of the check valve.

**6.7** If this test is to be conducted at the Phase I vapor coupler on a two-point Phase I system, the procedures set forth in subsections 6.7.1 and 6.7.2 shall be successfully completed prior to testing. The static pressure integrity test shall not be conducted at the Phase I coupler at facilities equipped with coaxial Phase I systems.

**6.7.1** Connect the Vapor Coupler Integrity Assembly to the Phase I vapor coupler. Connect the Vapor Coupler Test Assembly. Connect the nitrogen supply to the assembly and carefully pressurize the internal volume of the assembly to two (2.0) inches H<sub>2</sub>O. Start the stopwatch. Record the final pressure after one minute.

**6.7.2** If the pressure after one minute is less than 0.25 inches H<sub>2</sub>O, the leak rate through the Phase I vapor poppet precludes conducting the static leak test at this location. If the pressure after one minute is greater than or equal to 0.25 inches H<sub>2</sub>O, the static leak test may be conducted at this location. This criteria assures a maximum leak rate through the Phase I vapor poppet of less than 0.0004 cubic feet per minute.

**6.7.3** Disconnect the Vapor Coupler Integrity Assembly from the Phase I vapor coupler. If the requirements of subsection 6.7.2 were met, connect the Vapor Coupler Test Assembly to the Phase I vapor coupler.

**6.7.4** As an alternate to the requirements of subsections 6.7.1 through 6.7.3, leak detection solution may be used to verify the absence of vapor leaks through the Phase I vapor poppet on two-point Phase I systems. This alternative leak check is valid only for two-point Phase I systems in which tanks are manifolded. The manifold may be at the vent pipes. Pressurize the system to two (2) inches H<sub>2</sub>O and use the leak detection solution to verify a zero leak (absence of bubbles) condition at one of the vapor poppets on the Phase I system.

**6.8** All pressure measuring device(s) shall be bench calibrated using either a reference gauge or incline manometer. Calibration shall be performed at 20, 50, and 80 percent of full scale. Accuracy shall be within two percent at each

of these calibration points. Calibrations shall be conducted on a frequency not to exceed 90 days.

- 6.9** Use the flowmeter to determine the nitrogen regulator delivery pressures which correspond to nitrogen flowrates of 1.0 and 5.0 CFM. These pressures define the allowable range of delivery pressures acceptable for this test procedure. Also record the regulator delivery pressure setting, and the corresponding nitrogen flowrate that will be used during the test. As an alternative, the flowmeter may be connected, in-line between the nitrogen supply regulator and Vapor Coupler Test Assembly, during the test.
- 6.10** Use Equation 9.2 to calculate the approximate time required to pressurize the system ullage to the initial starting pressure of two (2.0) inches H<sub>2</sub>O. This will allow the tester to minimize the quantity of nitrogen introduced into those systems which cannot comply with the static leak standards.
- 6.11** Attach the Vapor Coupler Test assembly to the Phase I poppet or the "T" connector assembly to the Phase II vapor riser. Read the initial pressure of the storage tank and underground piping. If the initial pressure is greater than 0.5 inches H<sub>2</sub>O, carefully bleed off the pressure, in accordance with all applicable safety procedures, in the storage tank and underground piping to less than 0.5 inches H<sub>2</sub>O column.

## 7. TESTING

- 7.1** Open the nitrogen gas supply valve and set the regulator delivery pressure within the allowable range determined in Section 6.9, and start the stopwatch. Pressurize the vapor system (or subsystem for individual vapor return line systems) to **at least 2.2 inches H<sub>2</sub>O** initial pressure. It is critical to maintain the nitrogen flow until the pressure stabilizes, indicating temperature and vapor pressure stabilization in the tanks. Check the test equipment using leak detecting solution or a combustible gas detector to verify that all test equipment is leak tight.
  - 7.1.1** If the time required to achieve the initial pressure of two (2.0) inches H<sub>2</sub>O exceeds twice the time derived from Equation 9.2, stop the test and use liquid leak detector, or a combustible gas detector, to find the leak(s) in the system. Failure to achieve the initial starting pressure within twice the time derived from Equation 9.2 demonstrates the inability of the system to meet the performance criteria. Repair or replace the faulty component(s) and restart the test pursuant to Section 7.1.
- 7.2** Close and disconnect the nitrogen supply. Start the stopwatch when the pressure has decreased to the initial starting pressure of two (2.0) inches H<sub>2</sub>O.
- 7.3** At one-minute intervals during the test, record the system pressure. After five minutes, record the final system pressure. See Table 3-I (or Equation 9.1) to determine the acceptability of the final system static pressure results. For intermediate values of ullage in Table 3-I, linear interpolation may be employed.

- 7.4** If the system failed to meet the criteria set forth in Table 3-I (or Equation 9.1), repressurize the system and check all accessible vapor connections using leak detector solution or a combustible gas detector. If vapor leaks in the system are encountered, repair or replace the defective component and repeat the test. Potential sources of leaks include nozzle check valves, pressure/vacuum relief valves, containment box drain valve assemblies, and plumbing connections at the risers.
- 7.4.1** If the facility fails to comply with the static leak test standards and the Phase I system utilizes a non-CARB-certified drain valve equipped containment box, which was installed prior to July 1, 1992, for which a CARB-certified replacement drain valve assembly is not marketed, the following two subsections shall apply:
- 7.4.1.1** The drain valve may be removed and the port plugged. Reset the system. If the facility complies with the static leak test standards under these conditions, the facility shall be considered complying with the requirements, provided that the manufacturer and model number of the containment box and the date of installation are submitted with the test results.
- 7.4.1.2** The criteria set forth in subsection 7.4.1.1 shall not apply after July 1, 1996.
- 7.5** After the remaining system pressure has been relieved, remove the "T" connector assembly and reconnect the vapor recovery hose, if applicable.
- 7.6** If the vapor recovery system utilizes individual vapor return lines, repeat the leak test for each gasoline grade. Avoid leaving any vapor return line open longer than is necessary to install or remove the "T" connector assembly.
- 7.7** If the containment box has a cover-actuated drain valve, repeat the test with the cover in place. In these cases clearly specify, on Form 3-1, which results represent the pressure integrity with and without the cover in place.

## **8. POST-TEST PROCEDURES**

- 8.1** Use Table 3-1 or Equation 9.1 to determine the compliance status of the facility by comparing the final five-minute pressure with the minimum allowable final pressure.

## **9. CALCULATIONS**

- 9.1** The minimum allowable five-minute final pressure, with an initial pressure of two (2.0) inches H<sub>2</sub>O, shall be calculated as follows:

[Equation 9-1]

$$P_f = 2e^{\frac{-500.887}{V}} \quad \text{if } N = 1-6$$

$$P_f = 2e^{\frac{-531.614}{V}} \quad \text{if } N = 7-12$$

$$P_f = 2e^{\frac{-562.455}{V}} \quad \text{if } N = 13-18$$

$$P_f = 2e^{\frac{-593.412}{V}} \quad \text{if } N = 19-24$$

$$P_f = 2e^{\frac{-624.483}{V}} \quad \text{if } N > 24$$

Where:

- N = The number of affected nozzles. For manifolded systems, N equals the total number of nozzles. For dedicated plumbing configurations, N equals the number of nozzles serviced by the tank being tested.
- $P_f$  = The minimum allowable five-minute final pressure, inches H<sub>2</sub>O
- V = The total ullage affected by the test, gallons
- e = A dimensionless constant approximately equal to 2.718
- 2 = The initial starting pressure, inches H<sub>2</sub>O

**9.2** The minimum time required to pressurize the system ullage from zero (0) to two (2.0) inches H<sub>2</sub>O gauge pressure shall be calculated as follows:

$$t_2 = \frac{V}{[1522]F} \quad \text{[Equation 9-2]}$$

Where:

- $t_2$  = The minimum time to pressurize the ullage to two inches H<sub>2</sub>O, minutes
- V = The total ullage affected by the test, gallons
- F = The nitrogen flowrate into the system, CFM
- 1522 = The conversion factor for pressure and gallons

**9.3** If the policy of the local District requires an allowable tolerance for testing error, the minimum allowable five-minute final pressure, including testing error, shall be calculated as follows:

$$P_{f-E} = 2 - \left[ 1 + \left( \frac{E}{100} \right) \right] \left[ 408.9 - (P_f + 406.9) \right] \quad \text{[Equation 9-3]}$$

Where:

- $P_{fE}$  = The minimum allowable five-minute final pressure including allowable testing error, inches H<sub>2</sub>O
- E = The allowable testing error, percent
- $P_f$  = The minimum allowable five-minute final pressure calculated in Equations 9-1 or 9-2, inches H<sub>2</sub>O
- 2 = The initial starting pressure, inches H<sub>2</sub>O
- 408.9 = Atmospheric pressure plus the initial starting pressure, inches H<sub>2</sub>O
- 406.9 = Atmospheric pressure, inches H<sub>2</sub>O

## 10. REPORTING

- 10.1 The calculated ullage and system pressures for each five-minute vapor recovery system test shall be reported as shown in Form 3-1. Be sure to include the Phase I system type (two-point or coaxial), the Phase II system type, whether the system is manifolded, and the one-minute pressures during the test.

**Executive Order G-70-179**

**TABLE 3-1**

**PRESSURE DECAY LEAK RATE CRITERIA**

**INITIAL PRESSURE OF 2 INCHES OF H<sub>2</sub>O**

**MINIMUM PRESSURE AFTER 5 MINUTES, INCHES OF H<sub>2</sub>O**

<b><u>ULLAGE, GALLONS</u></b>	<b>NUMBER OF AFFECTED NOZZLES</b>				
	<b><u>01-06</u></b>	<b><u>07-12</u></b>	<b><u>13-18</u></b>	<b><u>19-24</u></b>	<b><u>&gt; 24</u></b>
<b>500</b>	<b>0.73</b>	<b>0.69</b>	<b>0.65</b>	<b>0.61</b>	<b>0.57</b>
550	0.80	0.76	0.72	0.68	0.64
<b>600</b>	<b>0.87</b>	<b>0.82</b>	<b>0.78</b>	<b>0.74</b>	<b>0.71</b>
650	0.93	0.88	0.84	0.80	0.77
<b>700</b>	<b>0.98</b>	<b>0.94</b>	<b>0.90</b>	<b>0.86</b>	<b>0.82</b>
750	1.03	0.98	0.94	0.91	0.87
<b>800</b>	<b>1.07</b>	<b>1.03</b>	<b>0.99</b>	<b>0.95</b>	<b>0.92</b>
850	1.11	1.07	1.03	1.00	0.96
<b>900</b>	<b>1.15</b>	<b>1.11</b>	<b>1.07</b>	<b>1.03</b>	<b>1.00</b>
950	1.18	1.14	1.11	1.07	1.04
<b>1,000</b>	<b>1.21</b>	<b>1.18</b>	<b>1.14</b>	<b>1.10</b>	<b>1.07</b>
1,200	1.32	1.28	1.25	1.22	1.19
<b>1,400</b>	<b>1.40</b>	<b>1.37</b>	<b>1.34</b>	<b>1.31</b>	<b>1.28</b>
1,600	1.46	1.43	1.41	1.38	1.35
<b>1,800</b>	<b>1.51</b>	<b>1.49</b>	<b>1.46</b>	<b>1.44</b>	<b>1.41</b>
2,000	1.56	1.53	1.51	1.49	1.46
<b>2,200</b>	<b>1.59</b>	<b>1.57</b>	<b>1.55</b>	<b>1.53</b>	<b>1.51</b>
2,400	1.62	1.60	1.58	1.56	1.54
<b>2,600</b>	<b>1.65</b>	<b>1.63</b>	<b>1.61</b>	<b>1.59</b>	<b>1.57</b>
2,800	1.67	1.65	1.64	1.62	1.60
<b>3,000</b>	<b>1.69</b>	<b>1.68</b>	<b>1.66</b>	<b>1.64</b>	<b>1.62</b>
3,500	1.73	1.72	1.70	1.69	1.67
<b>4,000</b>	<b>1.76</b>	<b>1.75</b>	<b>1.74</b>	<b>1.72</b>	<b>1.71</b>
4,500	1.79	1.78	1.77	1.75	1.74
<b>5,000</b>	<b>1.81</b>	<b>1.80</b>	<b>1.79</b>	<b>1.78</b>	<b>1.77</b>
6,000	1.84	1.83	1.82	1.81	1.80
<b>7,000</b>	<b>1.86</b>	<b>1.85</b>	<b>1.85</b>	<b>1.84</b>	<b>1.83</b>
8,000	1.88	1.87	1.86	1.86	1.85
<b>9,000</b>	<b>1.89</b>	<b>1.89</b>	<b>1.88</b>	<b>1.87</b>	<b>1.87</b>
10,000	1.90	1.90	1.89	1.88	1.88
<b>15,000</b>	<b>1.93</b>	<b>1.93</b>	<b>1.93</b>	<b>1.92</b>	<b>1.92</b>
20,000	1.95	1.95	1.94	1.94	1.94
<b>25,000</b>	<b>1.96</b>	<b>1.96</b>	<b>1.96</b>	<b>1.95</b>	<b>1.95</b>

**Note:** For manifolded Phase II Assist Systems, the "Number of Affected Nozzles" shall be the total of all gasoline nozzles. For dedicated return configurations, the "Number of Affected Nozzles" shall be the total of those nozzles served by the tank being tested.

## Form 3-1

<b>Distribution:</b>	<b>Executive Order G-70-179</b> <b>Exhibit 3</b>	Report No.: _____ Test Date: _____ <u>Test Times:</u> Run A: _____ Run B: _____ Run C: _____
<b>Summary of Source Test Results</b>		
<b>Source Information</b>		<b>Facility Parameters</b>
GDF Name and Address _____ _____ _____	GDF Representative and Title _____ _____ GDF Phone No. (    ) _____	PHASE I SYSTEM TYPE ( Check One) Two Point <input type="checkbox"/> Coaxial <input type="checkbox"/> Coaxial with Spill Prevention <input type="checkbox"/>
Permit Conditions _____	Source: GDF Vapor Recovery System GDF # _____ A/C # _____	PHASE II SYSTEM TYPE Catlow ICVN-VI <input type="checkbox"/> Manifolded? <b>Y</b> or <b>N</b>
<b>Operating Parameters:</b> Number of Nozzles Served by Tank #1 _____      Number of Nozzles Served by Tank #3 _____ Number of Nozzles Served by Tank #2 _____      Total Number of Gas Nozzles at Facility _____		
<b>Applicable Regulations:</b>		FOR OFFICE USE ONLY:

**Source Test Results and Comments:**

<u>TANK #:</u>	1	2	3	TOTAL
1. Product Grade	_____	_____	_____	_____
2. Actual Tank Capacity, Gallons	_____	_____	_____	_____
3. Gasoline Volume, Gallons	_____	_____	_____	_____
4. Ullage, Gallons (#2 -#3)	_____	_____	_____	_____
5. Phase I System Type	_____	_____	_____	_____
6. Initial Test Pressure, Inches H <sub>2</sub> O (2.0)	_____	_____	_____	_____
7. Pressure After 1 Minute, Inches H <sub>2</sub> O	_____	_____	_____	_____
8. Pressure After 2 Minutes, Inches H <sub>2</sub> O	_____	_____	_____	_____
9. Pressure After 3 Minutes, Inches H <sub>2</sub> O	_____	_____	_____	_____
10. Pressure After 4 Minutes, Inches H <sub>2</sub> O	_____	_____	_____	_____
11. <b>Final Pressure After 5 Minutes, Inches H<sub>2</sub>O</b>	_____	_____	_____	_____
12. Allowable Final Pressure from Table 3-1	_____	_____	_____	_____
13. Test Status [ <b>Pass</b> or <b>Fail</b> ]	_____	_____	_____	_____

Test Conducted by:	Test Company Name _____ Address _____ City _____	Date and Time of Test:
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## Executive Order G-70-179

### Exhibit 4

#### TEN GALLON PER MINUTE LIMITATION COMPLIANCE VERIFICATION PROCEDURE

Compliance with the 10 gallon per minute flowrate limitation shall be determined with the following methodology. It is recommended that the maximum dispensing rate through each nozzle/hose assembly be verified.

##### 1) The facility uses identical models of hoses, nozzles, and breakaways:

Check the nozzle closest to the submersible turbine pump (STP) for each gas grade, or STP, at the facility. With no other dispensing occurring which uses the same STP, dispense gas into a vehicle or approved container. Dispensing shall be conducted in the "hand-held, wide-open" mode. Using a stopwatch accurate to at least 0.2 seconds, begin timing the dispensing rate after at least one gallon has been dispensed. This one gallon buffer is necessary due to the "slow-start" nature of some dispensers. Determine the time required to dispense 2, 3, 4, or 5 gallons of gasoline. The facility shall be deemed in compliance with the 10 gallon per minute limitations if the elapsed time meets, or exceeds, the times shown in Table 1. If the dispensing rate exceeds the allowable limit, a CARB-certified flow limiting device shall be installed.

##### 2) The facility uses different models of hoses, nozzles, or breakaways

Due to potential differences in pressure drops through the various components, each of the nozzle/hose assemblies shall be tested for maximum dispensing rates. Using the same criteria as above, determine the maximum dispensing rate through each nozzle/hose assembly. If the maximum dispensing rate exceeds the 10 gpm limit, a CARB-certified flow limiting device shall be installed.

**Table 1**  
**Verification of 10 gpm**

Product Dispensed, gallons	Minimum Allowable Time, seconds
2.0	11.8
3.0	17.7
4.0	23.6
5.0	29.5

**Note: The times have been corrected to allow for the accuracy of the measurement.**